

MATH 3620  
Fluid Dynamics II

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Mondays 11am LT 11

Tuesdays 10am LT 18

[www.cbeaume.com](http://www.cbeaume.com)

Tutorials: W 3

or W 5

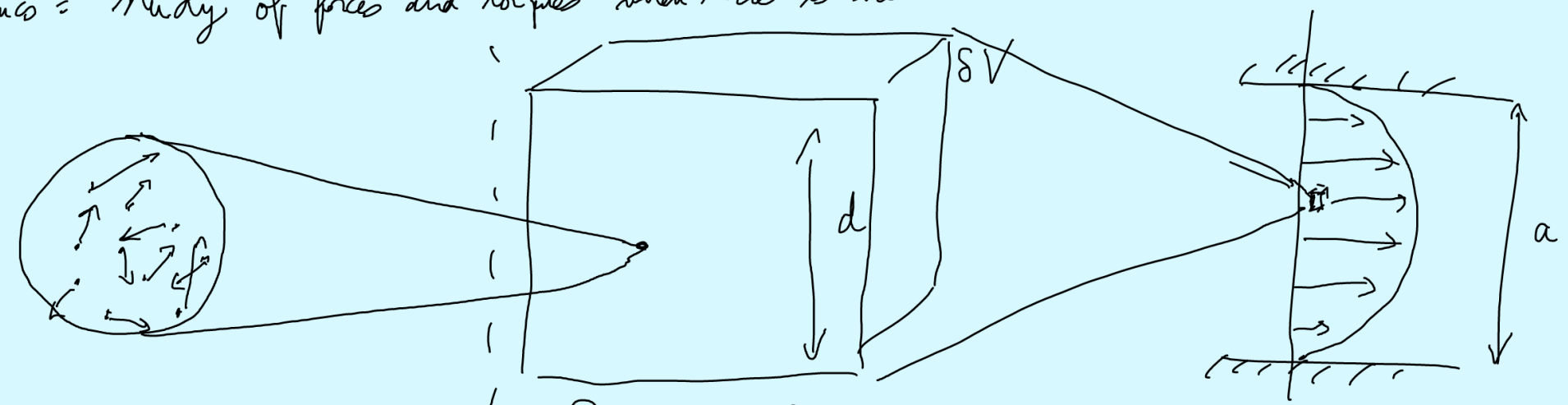
Tuesdays W 7

W 9

W 11

Fluid: substance that flows and takes the shape of its container.

Dynamics = study of forces and torques when there is motion

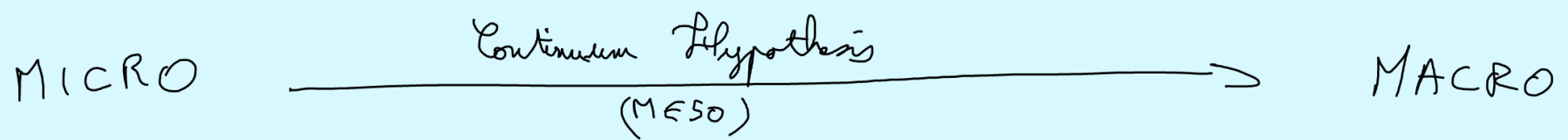


particle:  $\bar{V}_m = 1 \text{ \AA} = 10^{-10} \text{ m}$   
 ( $10^{23}$  water molecules per  $1 \text{ cm}^3$  of water)  
 mean free path:  $l_p = 10^{-8} \text{ m}$

{ element of fluid  
 fluid "particle"  
 blob of fluid }

$d \gg l_p$

$d \ll a$



$$\vec{v}(P, t) = \frac{\sum_{\text{particles in } SV} \vec{v}_{\text{particles}}}{\sum_{\text{particles in } SV} 1}$$

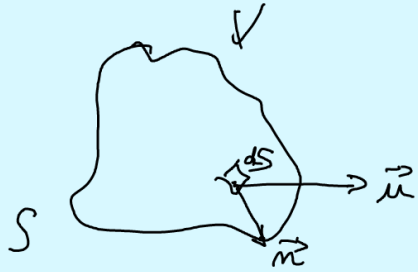
SV: blob of fluid centered on P.

$$\rho(P, t) = \frac{\sum_{\text{particles in } SV} m_{\text{particle}}}{SV}$$

watch Index Notation

# Conservation of mass

Lecture 2



$V$  is fixed  $\leftarrow$  volume of fluid

$\vec{n}$  unit vector: outward pointing normal

$$M_V = \int_V \rho \, dV \quad \text{total mass of fluid in } V$$

The rate of change of mass in time:  $\frac{dM_V}{dt} = \frac{d}{dt} \left( \int_V \rho \, dV \right)$

$$= \int_V \frac{d\rho}{dt} \, dV \quad \text{because } V \text{ is fixed}$$

Changes of mass of  $V$  are due to fluxes:

$$\frac{dM_V}{dt} = - \int_S \rho \vec{u} \cdot \vec{n} \, dS$$

$$\Rightarrow \int_V \frac{d\rho}{dt} \, dV = - \int_S \rho \vec{u} \cdot \vec{n} \, dS$$

$$\Rightarrow \int_V \frac{\partial \rho}{\partial t} dV = - \int_V \vec{\nabla} \cdot (\rho \vec{u}) dV \quad (\text{divergence theorem})$$

$$\Rightarrow \int_V \left[ \frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u}) \right] dV = 0$$

Because we did not impose any condition on the size of  $V$ , we can choose  $V$  to be infinitesimally small. In this case:

$$\boxed{\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u}) = 0} \quad \text{everywhere}$$

continuity equation  
mass conservation

Time derivative:  $\frac{\partial f}{\partial t}$ : rate of change in time of  $f$  at  $\vec{x}$  ← Euler

$$\frac{Df}{Dt}(\vec{x}(t), t) = \frac{\partial f}{\partial t} + \frac{\partial f}{\partial x} \frac{\partial x}{\partial t} + \frac{\partial f}{\partial y} \frac{\partial y}{\partial t} + \frac{\partial f}{\partial z} \frac{\partial z}{\partial t}$$

$$= \frac{\partial f}{\partial t} + u \frac{\partial f}{\partial x} + v \frac{\partial f}{\partial y} + w \frac{\partial f}{\partial z}$$

$$= \frac{\partial f}{\partial t} + (\vec{u} \cdot \vec{\nabla}) f \quad \text{rate of change in time of } f \text{ for a particle passing through } \vec{x} \text{ at } t$$

Lagrange



$$\left( \frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u}) = 0 \right) \Rightarrow \frac{\partial \rho}{\partial t} + \rho \vec{\nabla} \cdot \vec{u} + (\vec{u} \cdot \vec{\nabla}) \rho = 0$$

$$\Rightarrow \left( \frac{D\rho}{Dt} + \rho \vec{\nabla} \cdot \vec{u} = 0 \right)$$

Incompressibility condition: An incompressible fluid has  $\frac{D\rho}{Dt} = 0$

$$\text{Mass conservation} \Rightarrow \rho \vec{\nabla} \cdot \vec{u} = 0$$

$$\Rightarrow \boxed{\vec{\nabla} \cdot \vec{u} = 0} \text{ incompressibility } \left\{ \begin{array}{l} \text{condition} \\ \text{constraint} \end{array} \right.$$

This incompressibility condition impose a condition on the velocity.

$$\vec{\nabla} \cdot (\vec{\nabla} \times \vec{\psi}) = 0 \text{ always.}$$

So we can write  $\vec{u} = \vec{\nabla} \times \vec{\psi}$   $\vec{\psi}$  is the streamfunction

For example: a 2D flow:  $\vec{u} = u(x, y) \vec{e}_x + v(x, y) \vec{e}_y$

$$\Rightarrow \vec{\psi} = \psi(x, y) \vec{e}_z$$

$$u = \frac{\partial \psi}{\partial y}, \quad v = - \frac{\partial \psi}{\partial x}$$

Streamlines: lines where the streamfunction is constant

Lecture 3

$$d\psi = 0 \text{ on the streamline} \Rightarrow \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy = 0$$

$$\Rightarrow -v dx + u dy = 0$$

$$\Rightarrow \vec{u} \times d\vec{l} = 0 \quad \text{where } d\vec{l} = (dx, dy) \\ \text{element of displacement} \\ \text{along the streamline}$$

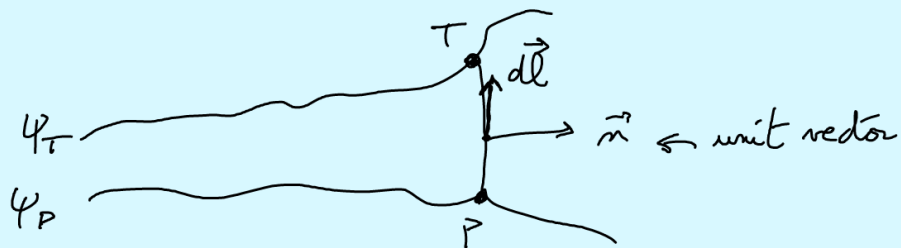
$$\Rightarrow \vec{u} \parallel \text{streamlines}$$

$$\vec{u} \cdot \nabla \psi = u \frac{\partial \psi}{\partial x} + v \frac{\partial \psi}{\partial y}$$

$$= \frac{\partial \psi}{\partial y} \frac{\partial \psi}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial \psi}{\partial y}$$

$$= 0 \quad (\text{same conclusion})$$

Flux between streamlines:



$$Q = \int_P^T \vec{u} \cdot \vec{n} ds$$

$$d\vec{l} = dx \vec{e}_x + dy \vec{e}_y$$

$$\vec{n} ds = dy \vec{e}_x - dx \vec{e}_y$$

$$= ds \left( \frac{dy}{ds} \vec{e}_x - \frac{dx}{ds} \vec{e}_y \right)$$

$$\begin{aligned}
\Rightarrow Q &= \int_P^T \left( u \frac{\partial y}{\partial s} - v \frac{\partial x}{\partial s} \right) ds \\
&= \int_P^T \left( \frac{\partial \psi}{\partial y} \frac{\partial y}{\partial s} + \frac{\partial \psi}{\partial x} \frac{\partial x}{\partial s} \right) ds \\
&= \int_P^T \frac{d\psi}{ds} ds \\
&= \int_P^T d\psi \\
&= \psi_T - \psi_P
\end{aligned}$$

$$\begin{aligned}
\|\vec{u}\| &= \left\| \frac{\partial \psi}{\partial y} \vec{e}_x - \frac{\partial \psi}{\partial x} \vec{e}_y \right\| \\
&= \left\| \left( \frac{\partial \psi}{\partial y}, -\frac{\partial \psi}{\partial x} \right) \right\| \\
&= \|\vec{\nabla} \psi\|
\end{aligned}$$

Strain rate and vorticity tensors:

velocity gradient tensor:  $\underline{\underline{K}}^{\leftarrow}$

$$K_{ij} = \frac{\partial u_i}{\partial x_j}$$

$$= E_{ij}$$

symmetric  
( $E_{ij} = E_{ji}$ )  
strain-rate tensor

$$+ \Omega_{ij}$$

anti-symmetric  
( $\Omega_{ij} = -\Omega_{ji}$ )  
vorticity tensor

$$E_{ij} = \frac{1}{2} (K_{ij} + K_{ji})$$

$$\Omega_{ij} = \frac{1}{2} (K_{ij} - K_{ji}) \leftarrow$$

2D flow incompressible:

$$\partial_x u + \partial_y v = 0$$

$$\Rightarrow \partial_x u = -\partial_y v$$

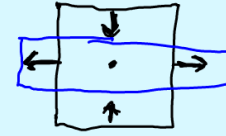
$$\bar{K} = \begin{pmatrix} \partial_x u & \partial_y u \\ \partial_x v & -\partial_x u \end{pmatrix}$$

3 unknowns

$$\hookrightarrow \bar{E} = \begin{pmatrix} a & b \\ b & -a \end{pmatrix}$$

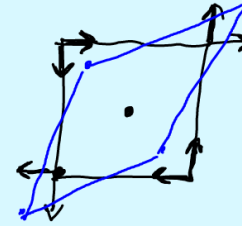
$$\bar{\Omega} = \begin{pmatrix} 0 & c \\ -c & 0 \end{pmatrix}$$

$$\cdot \bar{\bar{E}}_a = \begin{pmatrix} 1 & 0 \\ 0 & -1 \end{pmatrix} \quad \begin{array}{l} \underline{\underline{d_x u = 1}} \\ d_y v = -1 \end{array}$$



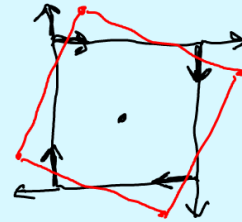
DEFORMATION

$$\cdot \bar{\bar{E}}_e = \begin{pmatrix} 0 & 1 \\ 1 & 0 \end{pmatrix} \quad \begin{array}{l} d_y u = 1 \\ d_x v = 1 \end{array}$$



DEFORMATION

$$\cdot \bar{\bar{\Omega}}_c = \begin{pmatrix} 0 & 1 \\ -1 & 0 \end{pmatrix} \quad \begin{array}{l} d_y u = 1 \\ d_x v = -1 \end{array}$$



SOLID BODY  
ROTATION

$\bar{\bar{E}}$  : deformation  $\rightarrow$  strain rate tensor

$\bar{\bar{\Omega}}$  : solid body rotation  $\rightarrow$  vorticity tensor

$$\vec{\omega} = \nabla \times \vec{u} \quad \text{vorticity}$$

$$\omega_i = \varepsilon_{ijk} \frac{\partial u_k}{\partial x_j}$$

$$\begin{aligned} \Rightarrow \frac{\varepsilon_{ilm} \omega_i}{\uparrow} &= \varepsilon_{ilm} \varepsilon_{ijk} \frac{\partial u_k}{\partial x_j} \\ &= \left( \delta_{lj} \delta_{mk} - \delta_{lk} \delta_{mj} \right) \frac{\partial u_k}{\partial x_j} \\ &= \frac{\partial u_m}{\partial x_l} - \frac{\partial u_l}{\partial x_m} \end{aligned}$$

$$= 2 \Omega_{ml} \leftarrow$$

$$\begin{aligned} \Rightarrow \Omega_{ml} &= \frac{1}{2} \varepsilon_{ilm} \omega_i \\ &= \frac{1}{2} \varepsilon_{klm} \omega_k \end{aligned}$$

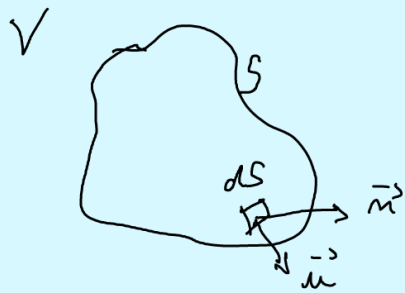
$$\begin{aligned} \Rightarrow \Omega_{ij} &= \frac{1}{2} \varepsilon_{kji} \omega_k \\ &= -\frac{1}{2} \varepsilon_{ijk} \omega_k \end{aligned}$$

$$\Omega_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right)$$

$$\vec{\Omega} = \begin{pmatrix} \pm \omega! & \pm \omega! \\ \dots & \dots \end{pmatrix}$$

# Chapter 2

## Equation of motion



$V$  fixed

$\vec{n}$ : unit outward pointing normal

momentum density  $\vec{q} = \rho \vec{u}$

total momentum in  $V$ :

$$\int_V \vec{q} dV$$

rate of change of the total momentum in  $V$  with time:  $\frac{d}{dt} \int_V \vec{q} dV = \int_V \frac{d\vec{q}}{dt} dV$

$$= \int_V \frac{d}{dt} (\rho \vec{u}) dV$$

Newton's second law:

$$\left( \begin{array}{c} \text{rate of change of} \\ \vec{q} \\ \text{in } V \\ \text{I} \end{array} \right) = \left( \begin{array}{c} \text{flux of } \vec{q} \\ \text{through } S \\ \text{II} \end{array} \right) + \left( \begin{array}{c} \text{net force} \\ \text{acting on } V \\ \text{III} \end{array} \right)$$

$$\cdot I_i = \int_V \frac{\partial}{\partial r} (\rho u_i) dV$$

$$\cdot II_i = - \int_S \vec{q} \cdot \vec{n} \cdot \vec{m} dS$$

$$\begin{aligned}
 \cdot II_i &= - \int_S q_i \underbrace{m_j}_{\vec{n}} dS \\
 &= - \int_V \frac{\partial}{\partial x_j} (\rho u_i u_j) dV \quad (\text{divergence theorem}) \\
 &= - \int_V \frac{\partial}{\partial x_j} (\rho u_i u_j) dV
 \end{aligned}$$

$$\cdot III_i = \int_V \vec{F}_{\text{body}} dV + \int_S \vec{F}_{\text{local}} dS$$

↙
↘

force density

$$\vec{F}_{\text{body}} = \rho \vec{g} \quad (+ \text{other})$$

$$F_{\text{body},i} = \rho g_i$$

$$F_{\text{local},i} = m_j \tau_{ji}$$

↙
↘

total stress tensor

$$\int_S F_{\text{local},i} dS = \int_S m_j \tau_{ji} dS$$



$$= \int_S \tau_{ji} n_j dS$$

$$= \int_V \frac{d}{dx_j} (\tau_{ji}) dV \quad (\text{divergence theorem})$$

$$\Rightarrow \int_V \frac{d}{dt} (\rho u_i) dV = - \int_V \frac{d}{dx_j} (\rho u_i u_j) dV + \int_V (\rho g_i) dV + \int_V \frac{d}{dx_j} (\tau_{ji}) dV$$

$$\Rightarrow \frac{d}{dt} (\rho u_i) + \frac{d}{dx_j} (\rho u_i u_j) = \rho g_i + \frac{d}{dx_j} (\tau_{ji}) \quad \text{pointwise (we can take } V \text{ as small as a "blob" of fluid)}$$

Continuity equation:  $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{u}) = 0$

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_j} (\rho u_j) = 0 \quad \leftarrow$$

$$\rho \frac{du_i}{dt} + \underbrace{u_i \left( \frac{\partial \rho}{\partial t} \right)} + \underbrace{u_i \frac{\partial}{\partial x_j} (\rho u_j)} + \rho u_i \frac{\partial}{\partial x_j} (u_i) = \rho g_i + \frac{d}{dx_j} (\tau_{ji})$$

$$\Rightarrow \rho \frac{du_i}{dt} + \rho \underbrace{u_j \frac{\partial}{\partial x_j}} u_i = \rho g_i + \frac{\partial}{\partial x_j} \tau_{ji}$$

$$\Rightarrow \boxed{\rho \left[ \frac{d\vec{u}}{dt} + (\vec{u} \cdot \vec{\nabla}) \vec{u} \right] = \rho \vec{g} + \vec{\nabla} \cdot \bar{\tau}}$$

momentum equation

Lecture 5

## 2.2 Constitutive equations

### 2.2.1 Ideal fluid

$\bar{\tau} = -P \bar{I}$  ← fluid in which the only internal stress is due to pressure.

$$\Rightarrow \tau_{ji} = -P \delta_{ij}$$

$$\begin{aligned} \Rightarrow \frac{\partial}{\partial x_j} \tau_{ji} &= - \frac{\partial P}{\partial x_j} \delta_{ij} \\ &= - \frac{\partial P}{\partial x_i} \end{aligned}$$

$$\Rightarrow \vec{\nabla} \cdot \bar{\tau} = - \vec{\nabla} P$$

$$\Rightarrow \boxed{\rho \left[ \frac{d\vec{u}}{dt} + (\vec{u} \cdot \vec{\nabla}) \vec{u} \right] = \rho \vec{g} - \vec{\nabla} P}$$

Euler equation

## 2.2.2 Newtonian fluids

Fluid for which the strain rate and the applied stress are linearly related ( $\rightarrow$  rheology).

Isotropic fluid (all directions expand similarly).

$$\vec{\tau} = -P\vec{I} + \vec{\sigma}$$

$\nwarrow$  viscous stress tensor

$$= -P\vec{I} + 2\mu \vec{E}$$

$\nwarrow$  strain rate tensor  
 $\nwarrow$  dynamic viscosity

$$\frac{\partial}{\partial x_j} \tau_{ji} = -\frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_j} \left[ 2\mu \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right]$$

$$= -\frac{\partial P}{\partial x_i} + \mu \frac{\partial}{\partial x_j} \left[ \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right]$$

$$= -\frac{\partial P}{\partial x_i} + \mu \frac{\partial^2 u_i}{\partial x_j^2} + \mu \frac{\partial^2 u_j}{\partial x_i \partial x_j}$$

$\rightarrow 0$  because  $\frac{\partial u_j}{\partial x_j} = 0$   
(incompressibility condition)

$$\Rightarrow \vec{\nabla} \cdot \vec{\tau} = -\vec{\nabla} P + \mu \vec{\nabla}^2 \vec{u}$$

$$\Rightarrow \rho \left[ \frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \vec{\nabla}) \vec{u} \right] = \rho \vec{g} - \vec{\nabla} P + \mu \vec{\nabla}^2 \vec{u}$$

Navier-Stokes equation

## 2.2.3 Different kinds of pressure

No flow, no forces: hydrostatic case:  $\vec{0} = \rho \vec{g} - \vec{\nabla} P_H$   $\leftarrow$  hydrostatic pressure

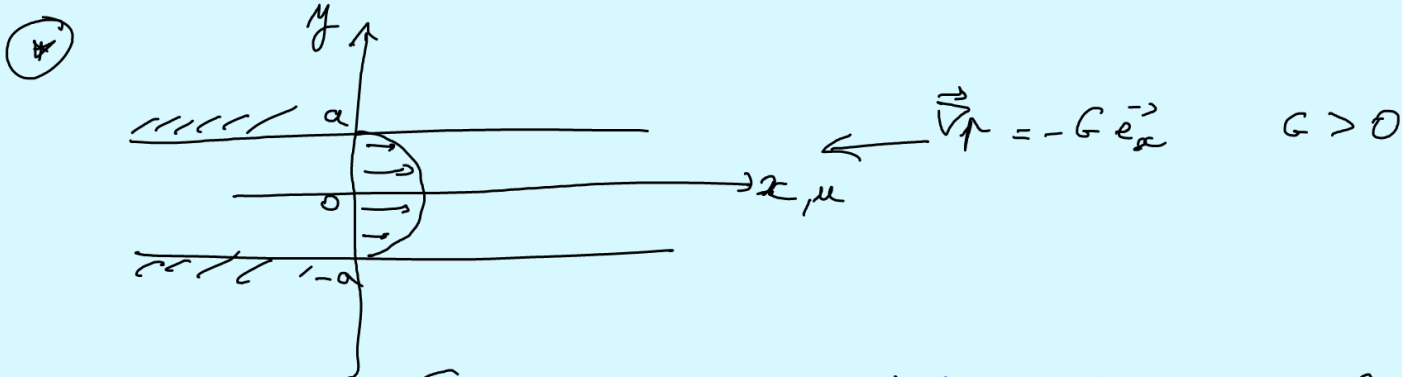
$$\Rightarrow P_H = \underbrace{\rho \vec{g} \cdot \vec{x}} + P_0 \leftarrow \text{reference pressure}$$

total  $\rightarrow P = P_H + p$   
 $\uparrow$  hydrostatic  $\uparrow$  dynamic pressure

pressure

$$\hookrightarrow \left[ \rho \left( \frac{d\vec{u}}{dt} + (\vec{u} \cdot \vec{\nabla}) \vec{u} \right) \right] = -\vec{\nabla} p + \mu \vec{\nabla}^2 \vec{u}$$

## Plane Poiseuille flow



Equations =

$$\begin{cases} \rho \frac{du}{dt} + \rho u \frac{du}{dx} + \rho v \frac{du}{dy} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2} \\ \rho \frac{dv}{dt} + \rho u \frac{dv}{dx} + \rho v \frac{dv}{dy} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2} \end{cases}$$

$$\left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \right)$$

⊕ Boundary conditions :

$y = a$	<del><math>v = 0</math></del> impermeability	$u = 0$ <u>no-slip</u>
$y = -a$	<del><math>v = 0</math></del>	$u = 0$

⊕ Hypothesis :

- steady flow :  $\frac{d}{dt} = 0$  .
- one dimensional :  $v = 0$  .

↳ Solution :

$$\left\{ \begin{array}{l} \rho u \frac{\partial u}{\partial x} = - \frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \rho \frac{\partial^2 u}{\partial y^2} \\ 0 = - \frac{\partial p}{\partial y} \\ \frac{\partial u}{\partial x} = 0 \end{array} \right. \longrightarrow u = u(y)$$

$$\Rightarrow \left\{ \begin{array}{l} \frac{\partial p}{\partial x} = \mu \frac{\partial u}{\partial y^2} \\ \frac{\partial p}{\partial y} = 0 \end{array} \right. \longrightarrow p = p(x)$$

$$\underbrace{\frac{\partial p}{\partial x}}_{f(x)} = \mu \underbrace{\frac{\partial u}{\partial y^2}}_{f(y)} = k_1 = -G$$

# Example Sheet 1

## Problem 1

$$\vec{v} = \begin{pmatrix} 4x + 2z \\ -4y \\ -2x \end{pmatrix}$$

$$(a) \begin{cases} \frac{dx}{dt} = 4x + 2z \\ \frac{dy}{dt} = -4y \\ \frac{dz}{dt} = -2x \end{cases} \Rightarrow \begin{cases} \frac{d^2x}{dt^2} = 4 \frac{dx}{dt} + 2 \frac{dz}{dt} = 4 \frac{dx}{dt} - 4z \\ \frac{dy}{dt} = -4y \\ y = k_1 e^{-4t} \end{cases} \quad \begin{aligned} \Delta &= 4^2 - 4(-4)^2 \\ &= 0 \\ x_{\pm} &= \frac{4 \pm \sqrt{0}}{2} \\ &= 2 \end{aligned}$$

$$\Rightarrow \begin{cases} x = (k_2 + k_3 t) e^{2t} \\ y = k_1 e^{-4t} \\ z = \frac{1}{2} \frac{dx}{dt} - 2x = \frac{1}{2} k_3 e^{2t} + (k_2 + k_3 t) e^{2t} - 2(k_2 + k_3 t) e^{2t} \\ = \underline{\underline{(-k_2 + \frac{1}{2} k_3 - k_3 t) e^{2t}}} \end{cases}$$

$$\begin{aligned} \text{at } t=0, \quad x &= x_0 \Rightarrow k_2 = x_0 \\ y &= y_0 \Rightarrow k_1 = y_0 \\ z &= z_0 \Rightarrow \underline{\underline{-k_2 + \frac{1}{2} k_3 = z_0}} \end{aligned}$$

$$\Rightarrow k_3 = 2(z_0 + x_0)$$

$$\Rightarrow \begin{cases} x = \left[ x_0 + \frac{2(z_0 + x_0)t}{1} \right] e^{2t} \\ y = y_0 e^{-4t} \\ z = \left[ z_0 - \frac{2(z_0 + x_0)t}{1} \right] e^{2t} \end{cases}$$

$$x y z = \left[ x_0 + 2(x_0 + z_0)t \right] y_0 \left[ z_0 - 2(x_0 + z_0)t \right]$$

$$\frac{2(x_0 + z_0)t}{x_0 y_0 z_0} = \frac{\left[ x_0 + 2(x_0 + z_0)t \right] \left[ z_0 - 2(x_0 + z_0)t \right]}{x_0 z_0}$$

$$\begin{aligned} \rightarrow \underline{x} + \underline{z} &= \left[ x_0 + z_0 \right] e^{2t} \\ y &= y_0 e^{-4t} \end{aligned}$$

$$\begin{aligned} x + z &= \left[ x_0 + 2(z_0 + x_0)t \right] e^{2t} + \left[ z_0 - 2(z_0 + x_0)t \right] e^{2t} \\ &= \left[ x_0 + 2(z_0 + x_0)t + z_0 - 2(z_0 + x_0)t \right] e^{2t} \\ &= \left[ x_0 + z_0 \right] e^{2t} \end{aligned}$$

$$\Rightarrow \boxed{(x+z)^2 y = (x_0 + z_0)^2 y_0}$$

$$\Rightarrow y = \frac{K}{(x+z)^2}, \quad K = (x_0 + z_0)^2 y_0$$

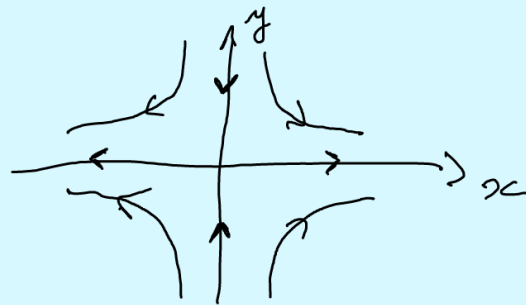
$$(c) \quad \vec{\nabla} \vec{u} = \begin{pmatrix} \frac{\partial u}{\partial x} & \frac{\partial u}{\partial y} & \frac{\partial u}{\partial z} \\ \frac{\partial v}{\partial x} & \frac{\partial v}{\partial y} & \frac{\partial v}{\partial z} \\ \frac{\partial w}{\partial x} & \frac{\partial w}{\partial y} & \frac{\partial w}{\partial z} \end{pmatrix} = \begin{pmatrix} 4 & 0 & 2 \\ 0 & -4 & 0 \\ -2 & 0 & 0 \end{pmatrix}$$

$$\vec{\Pi} = \begin{pmatrix} 4 & 0 & 0 \\ 0 & -4 & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

$$\vec{\Omega} = \begin{pmatrix} 0 & 0 & 2 \\ 0 & 0 & 0 \\ -2 & 0 & 0 \end{pmatrix}$$

$$\vec{\Pi} = \begin{pmatrix} 4 & 0 & 0 \\ 0 & -4 & 0 \\ 0 & 0 & 0 \end{pmatrix} \text{ only } \Rightarrow \begin{aligned} \frac{\partial u}{\partial x} &= 4 & u &= 4x + u_0 \\ \frac{\partial v}{\partial y} &= -4 & v &= -4y + v_0 \end{aligned}$$

To isolate the effect of  $\vec{E}$ , we set  $u_0 = v_0 = 0$





$$\Omega_{xz} = \begin{pmatrix} 0 & \ell \\ -2 & 0 \end{pmatrix}_{\text{only}} \Rightarrow \frac{\partial \mu}{\partial z} = 2$$

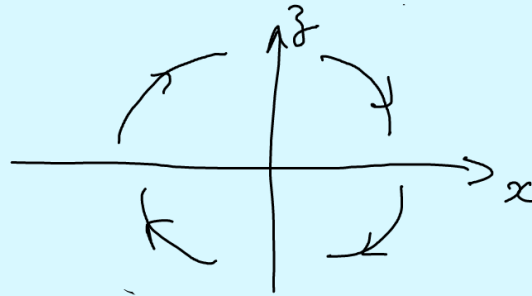
$$\mu = 2z + \mu_0$$

$$\frac{\partial w}{\partial z} = -2$$

$$w = -2x + w_0$$

$$\text{"} \dots \text{"} \Rightarrow \mu = 2z$$

$$w = -2x$$



### Problem 3

$$\vec{\nabla}^2 \vec{u} = \vec{\nabla} (\vec{\nabla} \cdot \vec{u}) - \vec{\nabla}_x (\vec{\nabla}_x \vec{u})$$

$$\vec{\nabla}_x (\vec{\nabla}_x \vec{u}) \Big|_i = \varepsilon_{ijk} \frac{\partial}{\partial x_j} (\vec{\nabla}_x \vec{u}) \Big|_k$$

$$= \varepsilon_{ijk} \frac{\partial}{\partial x_j} \left[ \varepsilon_{klm} \frac{\partial}{\partial x_l} u_m \right]$$

$$= \varepsilon_{ijk} \varepsilon_{klm} \frac{\partial}{\partial x_j} \left( \frac{\partial}{\partial x_l} u_m \right)$$

$$\begin{aligned}
&= \varepsilon_{kij} \varepsilon_{klm} \frac{\partial}{\partial x_j} \left( \frac{\partial}{\partial x_l} u_m \right) \\
&= (\delta_{il} \delta_{jm} - \delta_{im} \delta_{jl}) \frac{\partial}{\partial x_j} \left( \frac{\partial}{\partial x_l} u_m \right) \\
&= \delta_{il} \delta_{jm} \frac{\partial}{\partial x_j} \frac{\partial}{\partial x_l} u_m - \delta_{im} \delta_{jl} \frac{\partial}{\partial x_j} \frac{\partial}{\partial x_l} u_m \\
&= \frac{\partial}{\partial x_j} \frac{\partial}{\partial x_i} u_j - \frac{\partial}{\partial x_j} \frac{\partial}{\partial x_j} u_i \\
&= \frac{\partial}{\partial x_j} \left( \frac{\partial u_j}{\partial x_i} \right) - \frac{\partial^2}{\partial x_j^2} u_i
\end{aligned}$$

$$\hookrightarrow \vec{\nabla} \times (\vec{\nabla} \times \vec{u}) = \vec{\nabla} (\vec{\nabla} \cdot \vec{u}) - \vec{\nabla}^2 \vec{u}$$

$\Rightarrow \vec{\nabla}^2 \vec{u} = \vec{\nabla} (\vec{\nabla} \cdot \vec{u}) - \vec{\nabla} \times (\vec{\nabla} \times \vec{u})$ , which is what we were trying to prove.

$$\frac{\delta F}{\delta \alpha} = \mu \frac{\delta^2 u}{\delta y^2} = -G$$

$$\Rightarrow \frac{\delta^2 u}{\delta y^2} = -\frac{G}{\mu}$$

$$\Rightarrow u = -\frac{G}{2\mu} y^2 + k_2 y + k_3$$

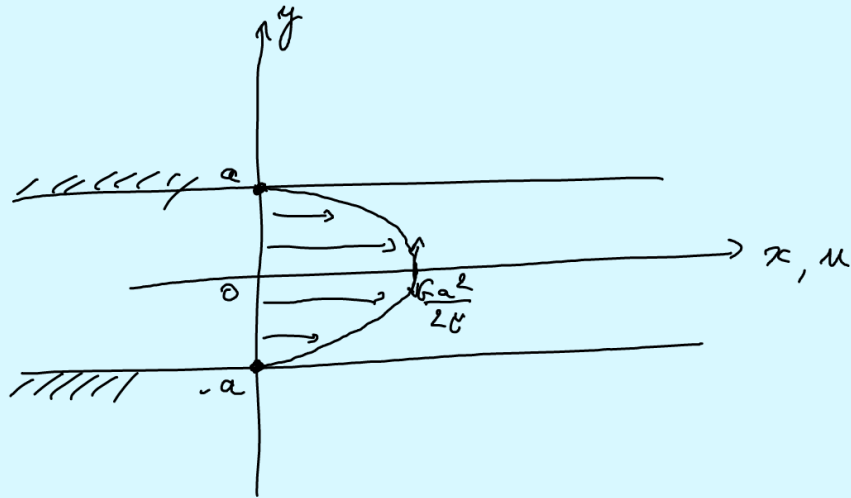
BC:  $y = a: u = 0 \Rightarrow 0 = -\frac{Ga^2}{2\mu} + k_2 a + k_3$

$y = -a: u = 0 \Rightarrow 0 = -\frac{Ga^2}{2\mu} - k_2 a + k_3$

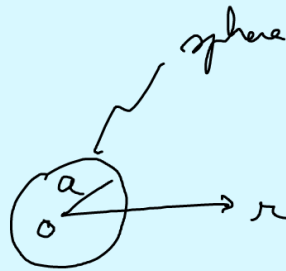
$$\Rightarrow k_2 = 0, k_3 = \frac{Ga^2}{2\mu}$$

$$\Rightarrow \boxed{u = \frac{G}{2\mu} [a^2 - y^2]}$$

⊕ Sketch:



2.6 The Reynolds number



$$\otimes \begin{cases} \rho \left[ \frac{d\vec{u}}{dt} + (\vec{u} \cdot \nabla) \vec{u} \right] = -\nabla p + \mu \nabla^2 \vec{u} \\ \nabla \cdot \vec{u} = 0 \end{cases}$$

BC: when  $r \rightarrow \infty$   $\vec{u} = U \vec{e}_x$   
 $r = a$   $\vec{u} = \vec{0}$

Non-dimensionalization:

$$\vec{x} = \alpha \vec{x}^*$$

$$[x] = L$$

$$[a] = L$$

$$[x^*] = 1 \rightarrow x^* \text{ is dimensionless}$$

$$\vec{u} = U \vec{u}^*$$

$$[u] = L \cdot T^{-1}$$

$$[U] = L \cdot T^{-1}$$

$$[u^*] = 1$$

$$t = \frac{a}{U} t^*$$

$$p = P \downarrow p^*$$

not the total pressure  
(the non-dimensionalizing pressure scale)

Into the equations:  $\nabla \cdot \vec{u} = 0 \Rightarrow \nabla \cdot (U \vec{u}^*) = 0$

$$\Rightarrow U \nabla \cdot (\vec{u}^*) = 0$$

$$\Rightarrow \frac{U}{\alpha} \nabla^* \cdot (\vec{u}^*) = 0$$

$$\Rightarrow \boxed{\nabla^* \cdot \vec{u}^* = 0}$$

$$\frac{\partial}{\partial x} = \frac{\partial}{\partial (\alpha x^*)} = \frac{1}{\alpha} \frac{\partial}{\partial x^*}$$

$$\rho \left[ \frac{U^2}{a} \frac{\partial \vec{u}^*}{\partial t^*} + \frac{U^2}{a} (\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^* \right] = -\frac{P}{a} \vec{\nabla}^* + \frac{\mu U}{a^2} \vec{\nabla}^{*2} \vec{u}^*$$

$$\Rightarrow \frac{\rho U^2}{a} \left[ \frac{\partial \vec{u}^*}{\partial t^*} + (\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^* \right] = -\frac{P}{a} \vec{\nabla}^* + \frac{\mu U}{a^2} \vec{\nabla}^{*2} \vec{u}^*$$

$$\Rightarrow \underbrace{\frac{\partial \vec{u}^*}{\partial t^*}}_{[\ ]=1} + \underbrace{(\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^*}_{[\ ]=1} = \underbrace{-\frac{P}{\rho U^2} \vec{\nabla}^*}_{[\ ]=1} + \underbrace{\frac{\mu}{\rho U a} \vec{\nabla}^{*2} \vec{u}^*}_{[\ ]=1}$$

$$[\vec{\nabla}^{*2} \vec{u}^*] = 1$$

$$\Rightarrow \left[ \frac{\mu}{\rho U a} \right] = 1$$

This is a nondimensional number

$Re = \frac{\rho U a}{\mu}$  is the Reynolds number

$$Re = \frac{\text{inertia}}{\text{viscous effects}}$$

$Re \gg 1 \rightarrow$  the flow is dominated by inertia

$Re \ll 1 \rightarrow$  the flow is dominated by viscous effects

$$\hookrightarrow \frac{d\vec{u}^*}{dt^*} + (\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^* = -\frac{P}{\rho U^2} \vec{\nabla}^* p^* + \frac{1}{\mathcal{R}e} \vec{\nabla}^{*2} \vec{u}^*$$

2 cases for  $P$ : \*  $P = \rho U^2$ :  $\frac{d\vec{u}^*}{dt^*} + (\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^* = -\vec{\nabla}^* p^* + \frac{1}{\mathcal{R}e} \vec{\nabla}^{*2} \vec{u}^*$ ,  $\vec{\nabla}^* \cdot \vec{u}^* = 0$

BC:  $r^* \rightarrow \infty$ ,  $\vec{u}^* = U \vec{e}_x$   
 $r^* = a r^*$

only 1 parameter

$r^* = 1$ ,  $\vec{u}^* = \vec{0}$

SIMILARITY THEORY

\*  $P = \frac{\mu U}{a}$   $\mathcal{R}e \left[ \frac{d\vec{u}^*}{dt^*} + (\vec{u}^* \cdot \vec{\nabla}^*) \vec{u}^* \right] = -\vec{\nabla}^* p^* + \vec{\nabla}^{*2} \vec{u}^*$ ,  $\vec{\nabla}^* \cdot \vec{u}^* = 0$

BC:  $r^* \rightarrow \infty$   $\vec{u}^* = U \vec{e}_x$   
 $r^* = 1$   $\vec{u}^* = \vec{0}$

# Chapter 3: Low Re flows

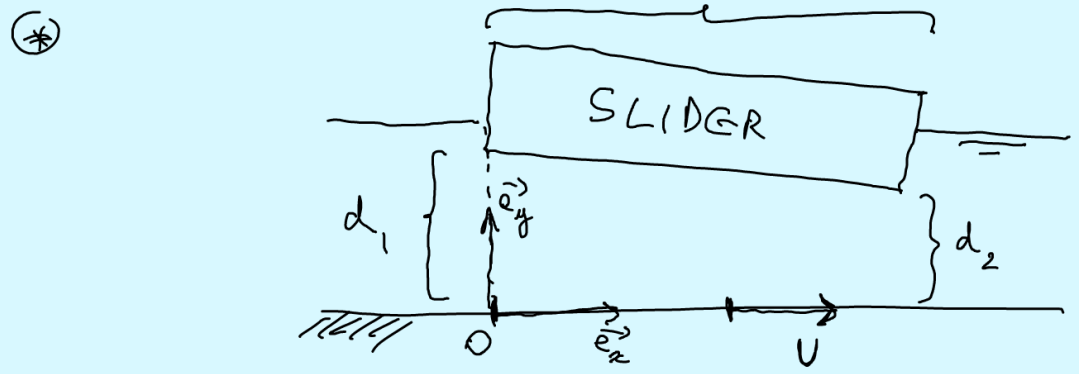
$$Re = \frac{\rho U a}{\mu} \ll 1$$

inertia  $\ll$  viscous effects, the flow is dominated by viscous effects.

Stokes flow

$$\begin{cases} \vec{\nabla} p = \mu \vec{\nabla}^2 \vec{u} & \text{Stokes equation} \\ \vec{\nabla} \cdot \vec{u} = 0 \end{cases}$$

## 3.3.1 Slider bearing flow



height of fluid between the slider and the wall

$$h(x) = d_1 + \frac{d_2 - d_1}{L} x$$

$$\bar{h} = \frac{d_1 + d_2}{2}$$

$$h' = \frac{dh}{dx}$$

$$|h'| \ll 1$$

Equations:

$$\begin{cases} \frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2} \\ \frac{\partial p}{\partial y} = \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2} \end{cases}$$



$$\left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \right)$$

- ⊙ BC.  $y=0$ :  $u=U$ ,  $v=0$   
 $y=h(x)$ :  $u=0$ ,  $v=0$

⊙ Hypothesis:  $|h'| \ll 1$  ←

- ⊙ Non-dimensionalization:  $x = \frac{x^*}{h}$   
 $y = h y^*$   
 $u = U u^*$   
 $v = V v^* = U h' v^* V$  to be determined  
 $\rho = P \rho^*$   $P$  to be determined



Look at  $h'$ :  $h' = \frac{dh}{dx} \begin{matrix} \rightarrow y \\ \rightarrow x \end{matrix}$   
 $\frac{1}{h'} = \frac{dx}{dh} \begin{matrix} \leftarrow x \\ \leftarrow y \end{matrix}$   
 $\frac{h}{h'} = h \frac{dx}{dh} \begin{matrix} \leftarrow x \\ \leftarrow y \end{matrix}$

⊙ Determination of  $V$  and  $P$ :

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \Rightarrow \frac{U h'}{h} \frac{\partial u^*}{\partial x^*} + \frac{V}{h} \frac{\partial v^*}{\partial y^*} = 0$$

$$\Rightarrow U h' \frac{\partial u^*}{\partial x^*} + V \frac{\partial v^*}{\partial y^*} = 0$$

$\Rightarrow V = U h'$  to allow the flow to be more complex than 1D.

$$\begin{cases} \frac{P h'}{h} \frac{\partial p^*}{\partial x^*} = \mu \left( \frac{U h'^2}{h^2} \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{U}{h^2} \frac{\partial^2 u^*}{\partial y^{*2}} \right) \\ \frac{P}{h} \frac{\partial p^*}{\partial y^*} = \mu \left( \frac{U h'^3}{h^2} \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{U h'}{h^2} \frac{\partial^2 v^*}{\partial y^{*2}} \right) \end{cases}$$

$$\Rightarrow \begin{cases} P \frac{\partial p^*}{\partial x^*} = \mu \left( \frac{U h'}{h} \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{U}{h h'} \frac{\partial^2 u^*}{\partial y^{*2}} \right) \\ P \frac{\partial p^*}{\partial y^*} = \mu \left( \frac{U h'^3}{h} \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{U h'}{h} \frac{\partial^2 v^*}{\partial y^{*2}} \right) \end{cases}$$

$$\Rightarrow \begin{cases} P \frac{\partial p^*}{\partial x^*} \approx \frac{\mu U}{h h'} \frac{\partial^2 u^*}{\partial y^{*2}} \rightarrow P = \frac{\mu U}{h h'} \\ P \frac{\partial p^*}{\partial y^*} \approx \frac{\mu U h'}{h} \frac{\partial^2 v^*}{\partial y^{*2}} \rightarrow P = \frac{\mu U h'}{h} \end{cases}$$

we use this scale because it is the largest, and therefore it includes the smallest contributions to the pressure

⊕ Recap:

$$x = \bar{h} h^{-1} x^*$$

$$y = \bar{h} y^* \leftarrow$$

$$u = U u^*$$

$$v = U h' v^*$$

$$p = \frac{\rho U}{\bar{h} h'} p^*$$

—  
scales

$$\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

$$\frac{\partial p^*}{\partial x^*} = \frac{\partial^2 u^*}{\partial y^{*2}}$$

$$\frac{\partial p^*}{\partial y^*} = 0$$

—  
equations

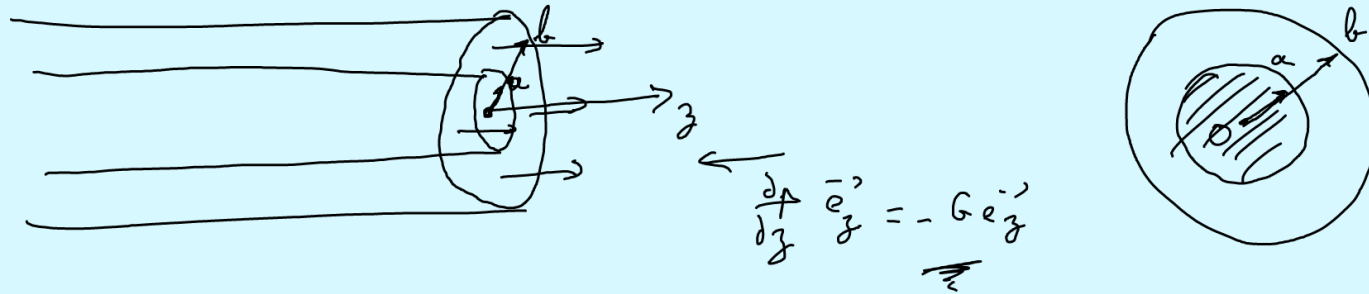
$$y^* = 0, \quad u^* = 1, \quad v^* = 0$$
$$y^* = h^*, \quad u^* = 0, \quad v^* = 0$$

$$h = \bar{h} a^*$$

—  
BC

EXAMPLE SHEET 2

3



$$\vec{u} = u \vec{e}_r + v \vec{e}_\theta + w \vec{e}_z$$

$$\Rightarrow \vec{u} = w(r) \vec{e}_z$$

Navier - Stokes in cylindrical coordinates :

$$\left. \begin{cases} 0 = -\frac{dp}{dz} \\ 0 = -\frac{1}{r} \frac{dp}{d\theta} \\ 0 = -\frac{dp}{dz} + \mu \left[ \frac{1}{r} \frac{d}{dr} \left( r \frac{dw}{dr} \right) \right] \end{cases} \right\} \Rightarrow p = p(z)$$

$\underbrace{\hspace{10em}}_{p(z)} \quad \underbrace{\hspace{10em}}_{f(r)}$

$$\frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial w}{\partial r} \right) = -\frac{G}{\mu} \Rightarrow r \frac{\partial w}{\partial r} = -\frac{Gr^2}{2\mu} + k_1$$

$$\Rightarrow \frac{\partial w}{\partial r} = -\frac{Gr}{2\mu} + \frac{k_1}{r}$$

$$\Rightarrow w = -\frac{Gr^2}{4\mu} + k_1 \ln r + k_2$$

$$\tau_{rz} = \begin{pmatrix} x & 0 & 0 \\ 0 & x & 0 \\ 0 & 0 & x \end{pmatrix}$$

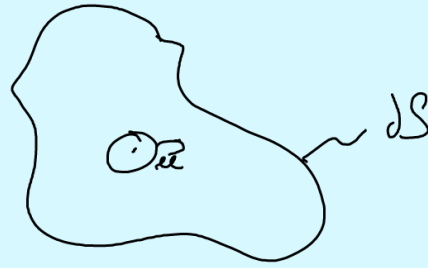
x normal stresses

o tangential stresses  $\rightarrow$  shear

Only component of the velocity gradient which is non-zero is  $\frac{\partial w}{\partial r}$

$$\tau_{rz} = \mu \frac{\partial w}{\partial r}$$

$$\textcircled{4} (a) \quad \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} = -\frac{G}{\mu} \quad (1)$$



$$(b) \quad \text{For } \frac{x^2}{a^2} + \frac{y^2}{b^2} = 1, \quad w \equiv 0$$

So, the velocity satisfies a no-slip boundary condition on the ellipse  $\frac{x^2}{a^2} + \frac{y^2}{b^2} = 1$

$$\text{Put in (1): } w = A \left( \frac{x^2}{a^2} + \frac{y^2}{b^2} - 1 \right)$$

$$\Rightarrow \frac{2A}{a^2} + \frac{2A}{b^2} = -\frac{G}{\mu}$$

$$\Rightarrow A \left( \frac{1}{a^2} + \frac{1}{b^2} \right) = -\frac{G}{2\mu}$$

$$\Rightarrow A = -\frac{G}{2\mu} \frac{a^2 b^2}{a^2 + b^2}$$

So, the velocity is, in fact:  $w = -\frac{G}{2\mu} \frac{a^2 b^2}{a^2 + b^2} \left( \frac{x^2}{a^2} + \frac{y^2}{b^2} - 1 \right)$

$$\text{If } a=b: w = -\frac{G a^2}{4\mu} \left( \frac{x^2}{a^2} + \frac{y^2}{a^2} - 1 \right)$$

$$\Rightarrow w = -\frac{G}{4\mu} (x^2 + y^2 - a^2)$$

$$\text{In polar coordinates } (r^2 = x^2 + y^2): w = \frac{G}{4\mu} (a^2 - r^2)$$

$$(c) w = B y \left[ (y - \sqrt{3} a)^2 - 3x^2 \right]$$

$$3 \text{ sides: } y = 0 \quad (i)$$

$$y = \sqrt{3} (a - x) \quad (ii)$$

$$y = \sqrt{3} (a + x) \quad (iii)$$

$$(i): w = B \cdot 0 \left[ \dots \right] = 0$$

$$(ii): w = B y \left[ \underbrace{(\sqrt{3} a - \sqrt{3} x - \sqrt{3} a)^2}_{\dots} - 3x^2 \right]$$

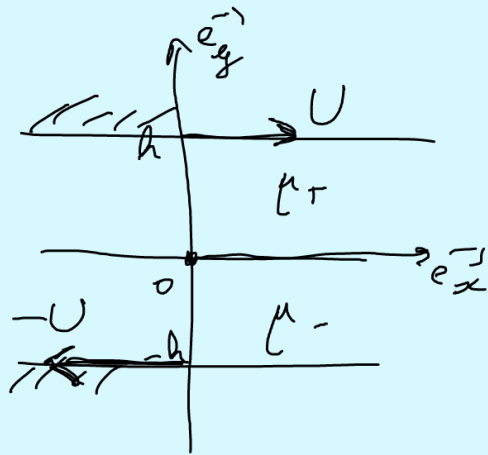
$$= B y \left[ 3x^2 - 3x^2 \right]$$

$$= 0$$

$$\begin{aligned}
 (iii) : w &= B y \left[ (\sqrt{3}a + \sqrt{3}x - \sqrt{3}a)^2 - 3x^2 \right] \\
 &= B y \left[ 3x^2 - 3x^2 \right] \\
 &= 0
 \end{aligned}$$

$\hookrightarrow$   $w = B y \left[ (y - \sqrt{3}a)^2 - 3x^2 \right]$  satisfies no-slip BC on the equilateral triangle with edges  $y=0$ ,  $y = \sqrt{3}(a-x)$ ,  $y = \sqrt{3}(a+x)$

②



$$(a) \quad u_+(y=0) = u_-(y=0)$$

$$\mu_+ \frac{\partial u_+}{\partial y}(y=0) = \mu_- \frac{\partial u_-}{\partial y}(y=0) \quad \checkmark$$

$$(b) \quad \vec{u} = u(y) \vec{e}_x$$

$$\hookrightarrow NS = \dots \dots \Rightarrow 0 = -\frac{d\mu}{dx} + \mu \frac{d^2 u}{dy^2}$$

$$\Rightarrow \frac{d^2 u}{dy^2} = 0$$



$$\frac{\partial^2 u_-}{\partial y^2} = 0$$

$$\Rightarrow u_- = k_1 y + k_2$$

$$\text{BC: } y = -h \quad u_- = -U$$

$$\Rightarrow u_- = k_1 y - U + k_1 h$$

$$\Rightarrow u_- = k_1 (y + h) - U$$

$$k_1 h - U = u_0$$

$$\Rightarrow k_1 = \frac{u_0 + U}{h}$$

$$\Rightarrow u_- = \frac{u_0 + U}{h} (y + h) - U$$

$$\frac{\partial^2 u_+}{\partial y^2} = 0$$

$$\Rightarrow u_+ = k_3 y + k_4$$

$$\text{BC: } y = h \quad u_+ = U$$

$$\Rightarrow u_+ = k_3 y + U - k_3 h$$

$$\Rightarrow u_+ = k_3 (y - h) + U$$

$$u_+(y=0) = u_-(y=0) = u_0$$

$$-k_3 h + U = u_0$$

$$\Rightarrow k_3 = \frac{U - u_0}{h}$$

$$u_+ = \frac{U - u_0}{h} (y - h) + U$$

$$\mu_- \frac{\partial u_-}{\partial y} \Big|_0 = \mu_+ \frac{\partial u_+}{\partial y} \Big|_0 \Rightarrow \mu_- \frac{u_0 + U}{h} = \mu_+ \frac{U - u_0}{h}$$

$$\Rightarrow \mu_-(u_0 + U) = \mu_+(U - u_0)$$

$$\Rightarrow \mu_0(\mu_- + \mu_+) = U(\mu_+ - \mu_-)$$

$$\Rightarrow \mu_0 = \frac{U(\mu_+ - \mu_-)}{\mu_+ + \mu_-}$$

$$x = \frac{\partial p}{\partial x^*}$$

$$y = \frac{\partial p}{\partial y^*}$$

$$c = \frac{\partial p}{\partial c^*}$$

$$r = \frac{\partial p}{\partial r^*}$$

$$p = \frac{\partial p}{\partial p^*}$$

$$\frac{\partial p}{\partial x^*} = \frac{\partial p}{\partial x^*} \quad \checkmark$$

$$\frac{\partial p}{\partial y^*} = 0 \quad \checkmark$$

$$\frac{\partial p}{\partial x^*} + \frac{\partial p}{\partial y^*} = 0 \quad \checkmark$$

$$y^* = 0$$

$$c^* = 1 \quad \checkmark$$

$$r^* = 0 \quad \checkmark$$

$$y^* = h^*$$

$$c^* = 0 \quad \checkmark$$

$$r^* = 0$$

Solution:  $p^* = p^*(x^*)$

$$c^* = \frac{1}{2} \frac{\partial p^*}{\partial x^*} y^{*2} + k_1 y^* + k_2$$

BC:  $y^* = 0, c^* = 1 \Rightarrow k_2 = 1$

$$y^* = h^*, c^* = 0 \Rightarrow \frac{1}{2} \frac{\partial p^*}{\partial x^*} h^{*2} + k_1 h^* + 1 = 0$$

$$\Rightarrow k_1 = -\frac{1}{h^*} - \frac{1}{2} \frac{\partial p^*}{\partial x^*} h^*$$

$$\underbrace{v^*}_{\leftarrow} \approx \frac{1}{2} \frac{\partial^2}{\partial x^2} \left[ y^{*2} - \frac{1}{2} y^* \right] + 1 - \underbrace{y^*}_{\leftarrow}$$

$$\frac{\partial^2}{\partial x^2} \left[ \frac{1}{2} y^{*2} - \frac{1}{2} y^* \right] + 1 - y^* = 0 \quad \left\{ \begin{array}{l} \frac{\partial^2}{\partial x^2} \left[ \frac{1}{2} y^{*2} - \frac{1}{2} y^* \right] \\ \leftarrow \frac{1}{2} \frac{\partial^2}{\partial x^2} (y^{*2}) \end{array} \right.$$

...

$$\Rightarrow v^*(y^*) = \frac{1}{2} \frac{\partial^2}{\partial x^2} \left( \frac{1}{2} y^{*2} - \frac{1}{2} y^* \right) + \frac{1}{4} \frac{\partial^2}{\partial x^2} y^{*2} - \frac{\partial^2}{\partial x^2} y^*$$

$$BC: y^* = 1 \Rightarrow v^* = 0$$

$$\Rightarrow \frac{1}{2} \frac{\partial^2}{\partial x^{*2}} f^{*3} + \frac{1}{4} \frac{\partial p^*}{\partial x^*} \frac{\partial h^*}{\partial x^*} h^{*2} - \frac{1}{2} \frac{\partial h^*}{\partial x^*} = 0$$

$$\Rightarrow \frac{\partial^2}{\partial x^{*2}} f^{*3} + 3 \frac{\partial p^*}{\partial x^*} \frac{\partial h^*}{\partial x^*} h^{*2} = 6 \frac{\partial h^*}{\partial x^*}$$

$$\Rightarrow \left( \frac{\partial}{\partial x^*} \left( \frac{\partial p^*}{\partial x^*} f^{*3} \right) \right) = 6 \frac{\partial h^*}{\partial x^*}$$

Reynolds equation

$$\hookrightarrow \frac{\partial p^*}{\partial x^*} = \frac{6}{h^{*2}} + \frac{k_w}{h^{*3}}$$

Note:  $h = a_1 + h'x \Rightarrow h^* = \frac{a_1}{h} + x^*$

$$\Rightarrow \frac{\partial h^*}{\partial x^*} = \frac{1}{h}$$

$$\int_0^L \frac{\partial p^*}{\partial x^*} dx^* = \int_0^L \left( \frac{6}{h^{*2}} + \frac{k_w}{h^{*3}} \right) dx^*$$

$$\vec{c}^* = \mathcal{W} \left[ \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*} \right] + \left( \gamma^* \sigma_1^* + \sigma_2^* \right) + \left( \gamma^* \sigma_1^* + \sigma_2^* \right)$$

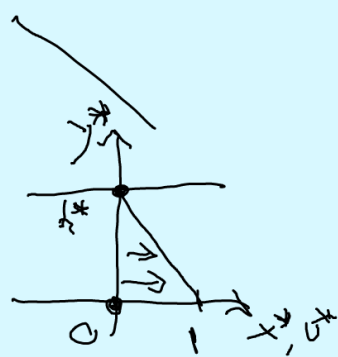
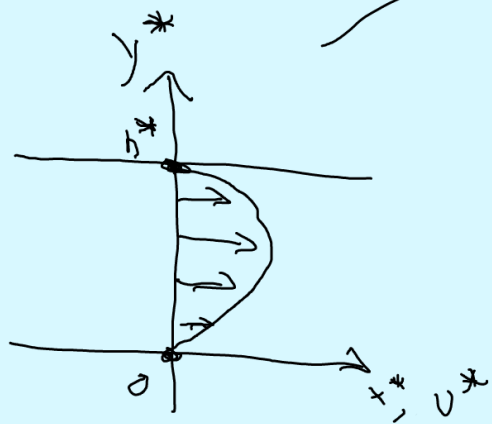
$$\vec{d}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*} \Rightarrow \vec{d}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*}$$

$$\vec{c}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*}$$

...

$$\vec{c}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*} \Rightarrow \vec{c}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*}$$

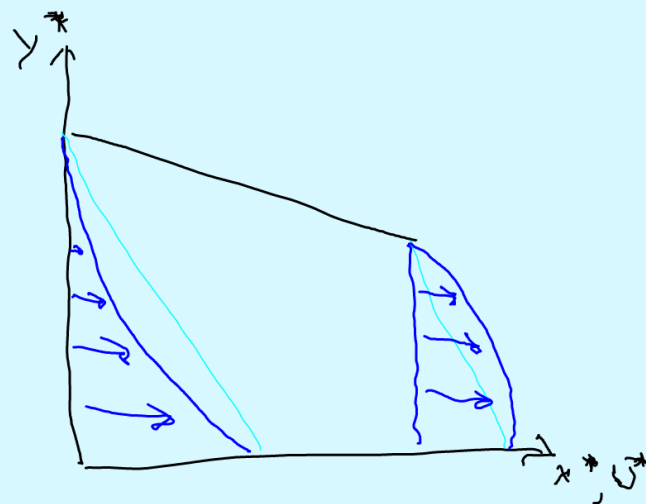
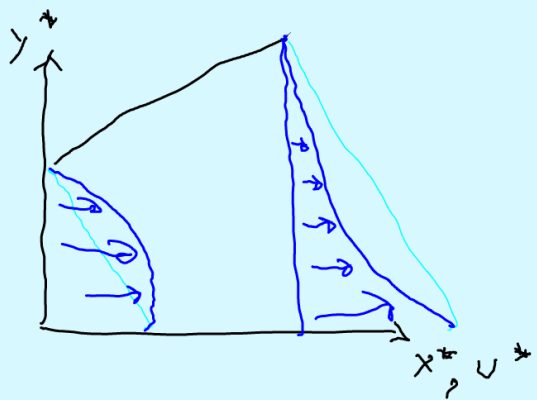
$$\vec{c}^* = \frac{2 \sigma_1^* \sigma_2^*}{\sigma_1^* + \sigma_2^*} + \left( \gamma^* \sigma_1^* + \sigma_2^* \right)$$



Note:  $d_1^* + d_2^* = 2$

$$\Rightarrow u^* = \omega \int_{-d_1^*}^{d_2^*} y^* dy^*$$

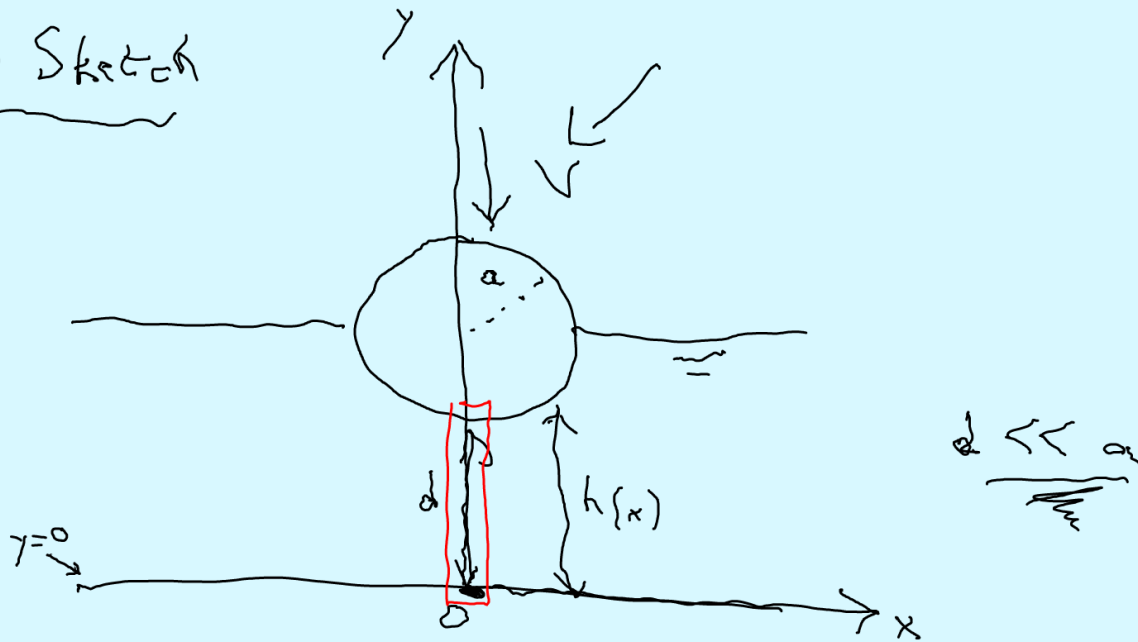
$$\left[ \frac{1}{2} \omega y^{*2} \right]_{-d_1^*}^{d_2^*} = \frac{1}{2} \omega (d_2^{*2} - d_1^{*2})$$



# Fluid expulsion between a cylinder and a well

Lecture 12

⊗ Sketch

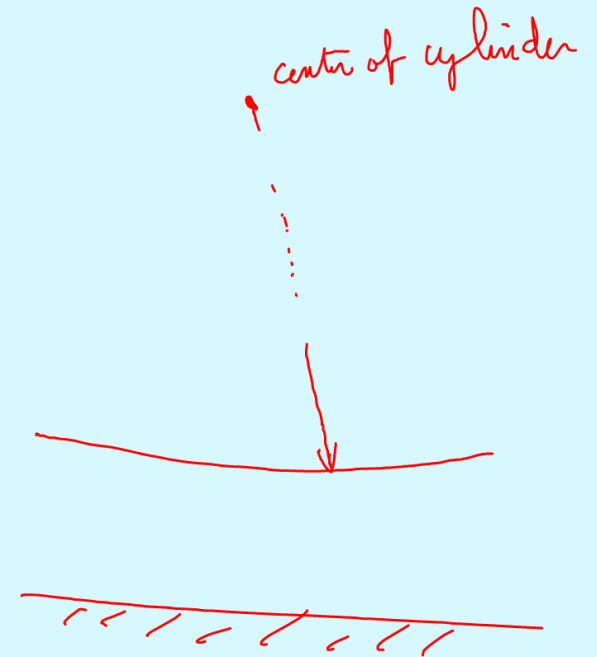


$$b(x) = d + a - \sqrt{a^2 - x^2}$$

$$= d + a - a \sqrt{1 - \frac{x^2}{a^2}}$$

$$\underbrace{x \ll a} \Rightarrow h(x) \approx d + a - a \left( 1 - \frac{x^2}{2a^2} \right)$$

$$\approx d \left( 1 + \frac{x^2}{2ad} \right)$$





⊗ Equations:

$$\begin{cases} \frac{\partial p}{\partial x} = \mu \left( \frac{\partial^2 u}{\partial x^2} + \nu \frac{\partial^2 u}{\partial y^2} \right) \\ \frac{\partial p}{\partial y} = \mu \left( \frac{\partial^2 v}{\partial x^2} + \nu \frac{\partial^2 v}{\partial y^2} \right) \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

⊗ BC:

$$y \leq 0: u = v = 0$$

$$y = h: u = 0, v = -V$$

⊗ Non-dimensionalization:

$$x = ? \cdot x^*$$

$$y = ? \cdot y^*$$

$$u = ? \cdot u^*$$

$$v = ? \cdot v^*$$

$$p = ? \cdot p^*$$

$$\frac{\partial^2 p}{\partial x^2} = \mu \left( \frac{\partial^2 v}{\partial x^2} + \nu \frac{\partial^2 v}{\partial y^2} \right) + \dots$$

$$x = \sqrt{a d} x^* = d \sqrt{\frac{a}{d}} x^* = d \varepsilon^{-1} x^* \quad m < 1$$

$$v = \sqrt{\varepsilon^{-1}} v^*$$

$$p = \frac{\mu \varepsilon^{-2}}{\rho} p^*$$

⊕ Recap:  $\frac{\partial p^*}{\partial x^*} = \frac{\partial^2 v^*}{\partial y^{*2}}$

$$\frac{\partial v^*}{\partial y^*} = 0$$

$$\frac{\partial v^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

$$y^* = 0, \quad v^* = v^* = 0$$

$$y^* = h^*, \quad v^* = 0, \quad v^* = -1$$

$$\text{Note: } h^* = 1 + \frac{1}{2} x^{*2}$$

⊕ Solution:

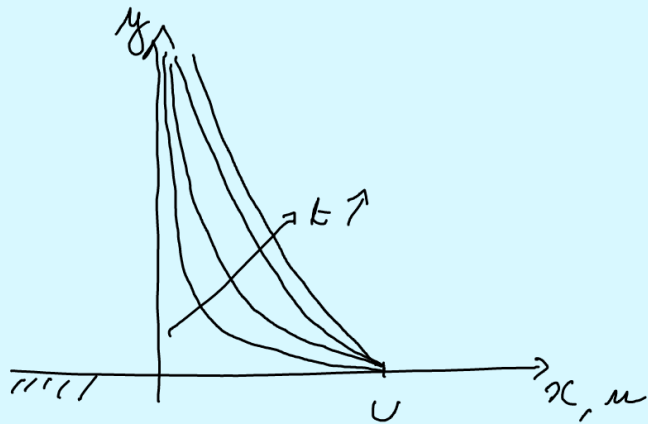
$$\frac{\partial}{\partial x^*} \left( \frac{\partial v^*}{\partial x^*} h^{*2} \right) = -12$$

Reynolds equation

# Chapter 4: Vorticity and boundary layers

Lecture 13

## 4.1.1 Stokes first problem



$$\begin{aligned} \textcircled{*} \quad y=0 &: v=0 \quad u=U \\ y \rightarrow \infty &: u \rightarrow 0 \quad v \rightarrow 0 \\ t=0 &: u=0 \quad v=0 \end{aligned}$$

$$\begin{aligned} \textcircled{*} \quad & \vec{u} = u(x, y, t) \vec{e}_x \quad \bullet \\ & \vec{\nabla}_p = \vec{0} \quad \bullet \end{aligned}$$

$$\text{Solution: } \begin{cases} \rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} \right) = - \frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \\ \frac{\partial p}{\partial y} = 0 \quad \rightarrow p(x) \\ \frac{\partial u}{\partial x} = 0 \quad \rightarrow u(y, t) \end{cases}$$

$$\textcircled{*} \begin{cases} \rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \\ \rho \left( \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = - \frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

$$\Rightarrow \rho \frac{\partial u}{\partial t} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial y^2}$$

$$\Rightarrow \rho \frac{\partial u}{\partial t} - \mu \frac{\partial^2 u}{\partial y^2} = -\frac{\partial p}{\partial x} = -G = 0$$

$$\Rightarrow \boxed{\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2}} \quad \nu = \frac{\mu}{\rho} \quad \text{kinematic viscosity}$$

$y=0 \quad u=U \quad \nu=0$   
 $y \rightarrow \infty \quad u \rightarrow 0 \quad \nu \rightarrow 0$   
 $t=0 \quad u=\nu=0$

(i) Separation of variables:  $u(y, t) = Y(y) T(t) \dots$

(ii) Similarity variable method:  $\begin{cases} \eta = y t^a \\ f(\eta) = u(y, t) \end{cases}$

$$\frac{\partial}{\partial t} = \frac{\partial}{\partial \eta} \frac{\partial \eta}{\partial t} = a t^{a-1} y \frac{\partial}{\partial \eta}$$

$$\frac{\partial}{\partial y} = \frac{\partial}{\partial \eta} \frac{\partial \eta}{\partial y} = t^a \frac{\partial}{\partial \eta} \quad \Rightarrow \quad \frac{\partial^2}{\partial y^2} = \frac{\partial}{\partial \eta} \left( \frac{\partial}{\partial \eta} \right) = \frac{\partial}{\partial \eta} \left( t^a \frac{\partial}{\partial \eta} \right)$$

$$= \frac{\partial}{\partial \eta} \frac{\partial \eta}{\partial y} \left( t^a \frac{\partial}{\partial \eta} \right)$$

$$= t^{2a} \frac{\partial^2}{\partial \eta^2}$$

$$\frac{\partial u}{\partial t} = v \frac{\partial^2 u}{\partial y^2} \Rightarrow a t^{a-1} y f' = v t^{2a} f''$$

$$\Rightarrow f'' = \frac{a t^{-a-1} y}{v} f'$$

$$y t^{-a-1} = \eta \Rightarrow y t^{-a-1} = y t^a$$

$$\Rightarrow t^{-2a-1} = 1$$

$$\Rightarrow -2a-1=0$$

$$\Rightarrow \boxed{a = -\frac{1}{2}}$$

$$\Rightarrow f'' = -\frac{\eta}{2v} f', \quad \underline{\eta = y t^{-1/2}} \quad (\eta = \frac{y}{\sqrt{t}})$$

+ BC

$$F = f'$$

$$F' = -\frac{\eta}{2v} F$$

$$\Rightarrow \frac{F'}{F} = -\frac{\eta}{2v}$$

$$\Rightarrow f' = k_1 \exp\left(-\frac{\eta^2}{4v}\right)$$

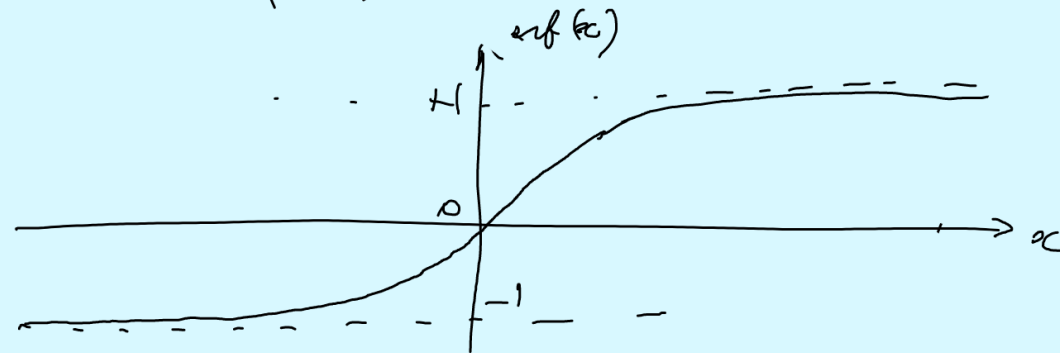
$$\Rightarrow f = k_1 \int_0^\eta \exp\left(-\frac{\xi^2}{4v}\right) d\xi + k_2$$

Error function:  $\text{erf}(x) = \frac{2}{\sqrt{\pi}} \int_0^x \exp(-y^2) dy$

$$y = \frac{\xi}{2\sqrt{v}} \quad \text{erf}(x) = \frac{2}{\sqrt{\pi}} \int_0^{2\sqrt{v}x} \exp\left(-\frac{\xi^2}{4v}\right) \frac{d\xi}{2\sqrt{v}}$$

$$2\sqrt{v}x = \eta \quad \text{erf}\left(\frac{\eta}{2\sqrt{v}}\right) = \frac{1}{\sqrt{\pi v}} \int_0^{\eta} \exp\left(-\frac{\xi^2}{4v}\right) d\xi$$

$$\hookrightarrow f = k_1 \sqrt{\pi v} \text{erf}\left(\frac{\eta}{2\sqrt{v}}\right) + k_2$$



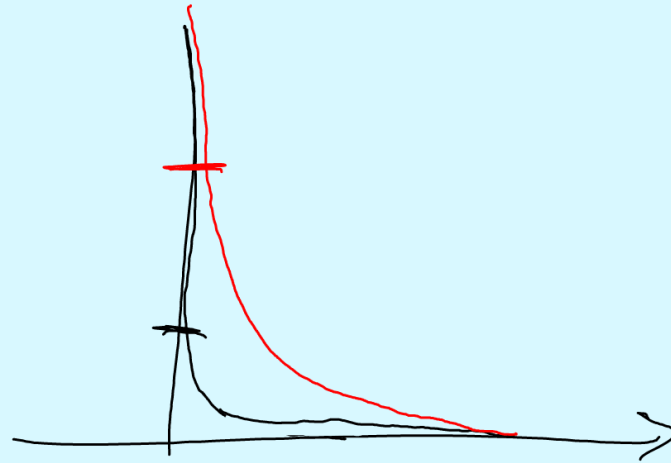
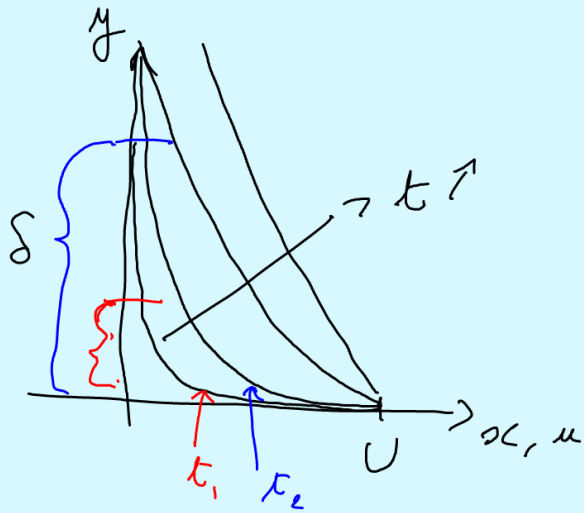
$$u = k_3 \text{erf}\left(\frac{y}{2\sqrt{v t}}\right) + k_2$$

BC:  $y=0 : u=U \quad \Rightarrow \quad k_2 = U$

$y \rightarrow \infty : u \rightarrow 0 \quad \Rightarrow \quad k_3 + k_2 = 0$   
 $\Rightarrow k_3 = -U$

$$u = U \left[ 1 - \operatorname{erf} \left( \frac{y}{\delta \sqrt{\nu t}} \right) \right]$$

IC:  $t=0$   $u=0$  which is compatible with the above solution.

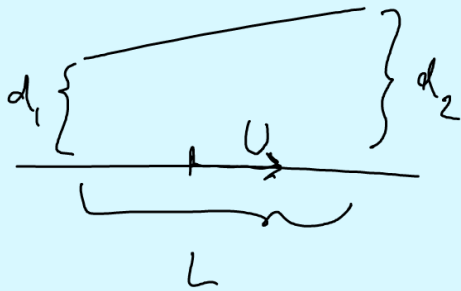


$\delta \sim \sqrt{\nu t}$  is the distance over which the effect of the moving wall is felt.  
 $\uparrow$  thickness of the boundary layer

$\operatorname{erf}(2) \approx 0.99 \Rightarrow \frac{\delta_{99}}{2\sqrt{\nu t}} = 2$  is the thickness of the boundary layer given by the 99% criterion

$$\Rightarrow \delta_{99} = 4\sqrt{\nu t}$$

# Problem 3



$$u \sim U$$

$$v \sim U h'$$

$$x \sim \bar{h}/h'$$

$$y \sim h$$

$$\rho u \frac{\partial u}{\partial x} \sim \rho \frac{U^2 h'}{h}$$

$$\rho v \frac{\partial u}{\partial y} \sim \rho \frac{U^2 h'}{h}$$

$$\rho u \frac{\partial v}{\partial x} \sim \rho \frac{U^2 h'^2}{h}$$

$$\rho v \frac{\partial v}{\partial y} \sim \rho \frac{U^2 h'^2}{h}$$

$$\rightarrow \rho \frac{U^2 h'^2}{h}$$

$$\rho \frac{U^2 h'^2}{h}$$

$$\rho (\vec{u} \cdot \nabla) \vec{u} \sim \rho \frac{U^2 h'}{h}$$

$$\rho \nabla^2 \vec{u}$$

$$\rho \frac{\partial^2 u}{\partial x^2} \sim \rho \frac{U U h'^2}{h^2}$$

$$\rho \frac{\partial^2 u}{\partial y^2} \sim \rho \frac{U U}{h^2}$$

$$\rho \frac{\partial^2 v}{\partial x^2} \sim \rho \frac{U U h'^3}{h^2}$$

$$\rho \frac{\partial^2 v}{\partial y^2} \sim \rho \frac{U U h'}{h^2}$$



Inertia is negligible provided:  $\rho \frac{U^2 h'}{h} \ll \frac{\mu U}{h^2}$

$$\Rightarrow U \ll \frac{\mu}{\rho h h'}$$

$$\Rightarrow U \ll \frac{\mu^2 L}{\rho (d_1 + d_2) (d_2 - d_1)}$$

$$\Rightarrow U \ll \frac{2\mu L}{\rho |d_2^e - d_1^e|}$$

$$\Rightarrow \frac{\rho U (d_1 + d_2)}{2\mu} \ll \frac{2\mu L}{\rho |d_2^e - d_1^e|} \quad \frac{\rho (d_1 + d_2)}{2\mu}$$

$$\Rightarrow Re \ll \frac{L (d_1 + d_2)}{|d_2^e - d_1^e|}$$

$$\Rightarrow Re \ll \frac{L}{|d_2 - d_1|}$$

↳ If  $|d_2 - d_1| \ll 1$ , then we can neglect inertia for large  $Re$ .

Vorticity equation

Navier-Stokes:  $\rho \left[ \frac{d\vec{u}}{dt} + (\vec{u} \cdot \nabla) \vec{u} \right] = -\nabla p + \mu \nabla^2 \vec{u}$

Incompressibility condition:  $\nabla \cdot \vec{u} = 0$

Note:  $\nabla \times \nabla \cdot \vec{F} = \vec{0}$  always (take cartesian example, or index notation, or vector calculus)

Remember from ES 1:  $\vec{u} \times (\nabla \times \vec{u}) = \frac{1}{2} \nabla(\vec{u}^2) - \underline{(\vec{u} \cdot \nabla) \vec{u}}$

$$\hookrightarrow \rho \left[ \frac{d\vec{u}}{dt} + \frac{1}{2} \nabla(\vec{u}^2) - \underbrace{\vec{u} \times (\nabla \times \vec{u})}_{\vec{\omega}} \right] = -\nabla p + \mu \nabla^2 \vec{u}$$

$$\Rightarrow \rho \left[ \frac{d\vec{u}}{dt} - \vec{u} \times \vec{\omega} \right] = -\nabla \left[ p + \frac{1}{2} \vec{u}^2 \right] + \mu \nabla^2 \vec{u}$$

We take the curl:  $\rho \frac{d\vec{\omega}}{dt} - \rho \nabla \times (\vec{u} \times \vec{\omega}) = \vec{0} + \mu \nabla^2 \vec{\omega}$

$$\nabla \times (\vec{u} \times \vec{\omega}) \Big|_i = \varepsilon_{ijk} \frac{d}{dx_j} (\vec{u} \times \vec{\omega})_k$$

$$= \varepsilon_{ijk} \frac{d}{dx_j} (\varepsilon_{klm} u_l \omega_m)$$

$$= \varepsilon_{kij} \varepsilon_{klm} \frac{d}{dx_j} (u_l \omega_m)$$

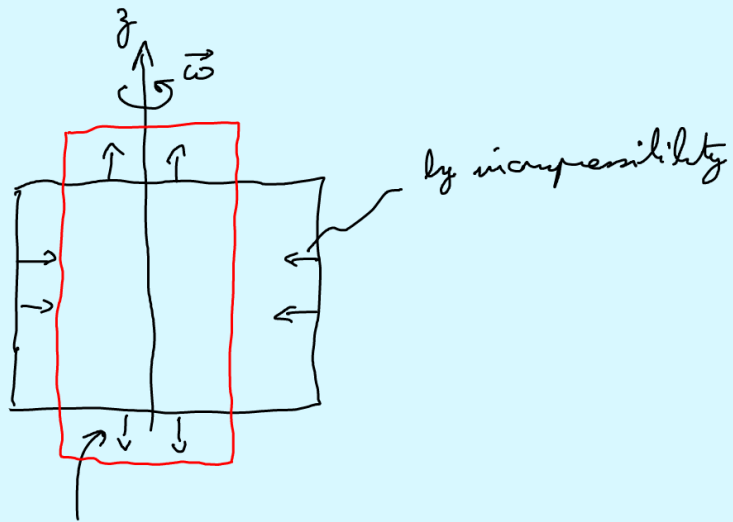
$$= (\delta_{ik} \delta_{jm} - \delta_{im} \delta_{jk}) \frac{d}{dx_j} (u_l \omega_m)$$



$$\Rightarrow \frac{\partial \omega}{\partial t} = \omega \frac{\partial}{\partial z} \omega$$

$$\Rightarrow \underbrace{\frac{1}{\omega} \frac{\partial \omega}{\partial t}} = \frac{\partial \omega}{\partial z}$$

relative rate  
of change of  
 $\omega$  with time

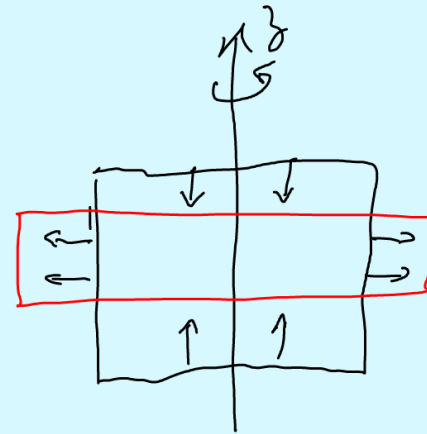


$$\frac{\partial \omega}{\partial z} > 0$$

$$\Rightarrow \frac{1}{\omega} \frac{\partial \omega}{\partial t} > 0$$

$$\Rightarrow |\omega| \nearrow$$

↳ blob of fluid gets thinner (and longer)  
and spins faster



$$\frac{\partial \omega}{\partial z} < 0$$

$$\Rightarrow \frac{1}{\omega} \frac{\partial \omega}{\partial t} < 0$$

$$\Rightarrow |\omega| \searrow$$

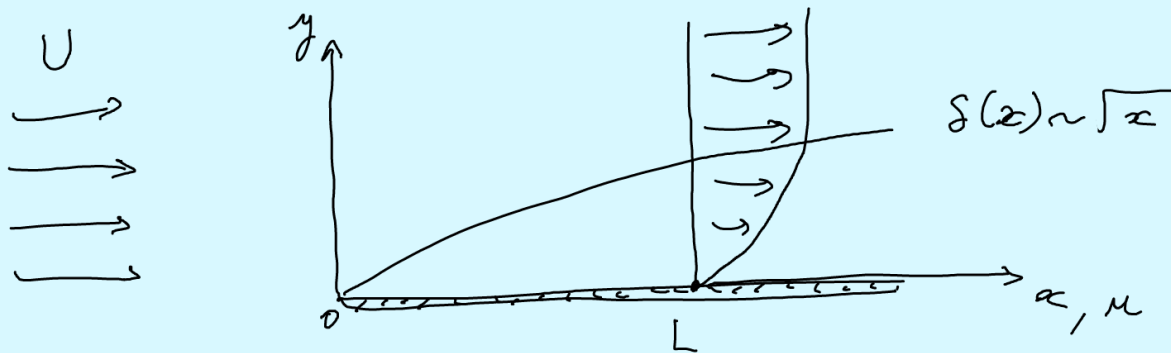
↳ blob of fluid becomes wider (and shorter)  
and spins more slowly.

Remark: 2D flow  $\rightarrow \vec{u} = u(x, y) \vec{e}_x + v(x, y) \vec{e}_y$   
 $\Rightarrow \vec{\omega} = \omega(x, y) \vec{e}_z$

$$\rho \left[ \frac{d\vec{\omega}}{dt} + (\vec{u} \cdot \nabla) \vec{\omega} \right] = \rho (\vec{\omega} \cdot \nabla) \vec{u} + \mu \nabla^2 \vec{\omega}$$

$$\Rightarrow \rho \left[ \frac{d\omega}{dt} + (\vec{u} \cdot \nabla) \omega \right] = \mu \nabla^2 \omega$$

Blasius boundary layer



(\* Hypotheses:

- 2D
  - steady
  - large  $Re = \frac{\rho U L}{\mu} \gg 1$
  - thin BL:  $\frac{\delta}{L} = \epsilon \ll 1$
- $\frac{\rho U L}{\mu} \gg 1 \rightarrow L \gg \frac{\mu}{\rho U}$

(\* Equations:

$$\begin{cases} \rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2} \\ \rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2} \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

3 state variables  
(u, v, p)  
2D problem (x, y)

(\* BC:

$$\begin{aligned} y=0: & \quad u=v=0 \\ y \rightarrow \infty: & \quad u \rightarrow U, v \rightarrow 0 \end{aligned}$$

(\* Nondimensionalization:

$$\begin{aligned} x &= L x^* \\ y &= \delta y^* = \epsilon L y^* \\ u &= U u^* \\ v &= U \epsilon v^* \leftarrow \text{incompressibility condition} \\ p &= \rho U^2 p^* \end{aligned}$$

$$\hookrightarrow \begin{cases} \rho \frac{U^2}{L} u^* \frac{\partial u^*}{\partial x^*} + \rho \frac{U^2}{L} v^* \frac{\partial u^*}{\partial y^*} = -\rho \frac{U^2}{L} \frac{\partial p^*}{\partial x^*} + \frac{\mu U}{L^2} \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{\mu U}{\varepsilon^2 L^2} \frac{\partial^2 u^*}{\partial y^{*2}} \\ \rho \frac{\varepsilon U^2}{L} u^* \frac{\partial v^*}{\partial x^*} + \rho \frac{\varepsilon U^2}{L} v^* \frac{\partial v^*}{\partial y^*} = -\rho \frac{U^2}{\varepsilon L} \frac{\partial p^*}{\partial y^*} + \frac{\mu \varepsilon U}{L^2} \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{\mu U}{\varepsilon L^2} \frac{\partial^2 v^*}{\partial y^{*2}} \\ \frac{U}{L} \frac{\partial u^*}{\partial x^*} + \frac{\varepsilon U}{\varepsilon L} \frac{\partial v^*}{\partial y^*} = 0 \end{cases}$$

$$\Rightarrow \begin{cases} \overbrace{u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial u^*}{\partial y^*}}^{\text{inertia}} = -\frac{\partial p^*}{\partial x^*} + \cancel{\frac{1}{\text{Re}_L} \frac{\partial^2 u^*}{\partial x^{*2}}} + \frac{1}{\varepsilon^2 \text{Re}_L} \frac{\partial^2 u^*}{\partial y^{*2}} \\ \cancel{u^* \frac{\partial v^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*}} = -\frac{1}{\varepsilon^2} \frac{\partial p^*}{\partial y^*} + \cancel{\frac{1}{\text{Re}_L} \frac{\partial^2 v^*}{\partial x^{*2}}} + \frac{1}{\varepsilon^2 \text{Re}_L} \frac{\partial^2 v^*}{\partial y^{*2}} \\ \frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0 \end{cases} \quad \text{Re}_L = \frac{\rho U L}{\mu}$$

to keep inertia and diffusion in balance, we require  $\varepsilon^2 \text{Re}_L = 1$

$$\hookrightarrow \text{Re} = \varepsilon^{-2}$$

$$\Rightarrow \frac{\rho U L}{\mu} = \frac{L^2}{\delta^2}$$

$$\Rightarrow \delta = \sqrt{\frac{L \mu}{\rho U}}$$

$$\Rightarrow \begin{cases} \rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial y^2} \\ \frac{\partial p}{\partial y} = 0 \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

Since  $\frac{\partial p}{\partial y} = 0$ , we can get the pressure from a streamline located infinitely far away from the BL.

$$\hookrightarrow p + \frac{1}{2} \rho U_a^2 = \text{const}$$

$$\Rightarrow p = \text{const}$$

$$\Rightarrow \frac{\partial p}{\partial x} = 0$$

$$\hookrightarrow \begin{cases} \rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \mu \frac{\partial^2 u}{\partial y^2} \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

2 state variables ( $u, v$ )

2D ( $x, y$ )



Streamfunction:  $u = \frac{\partial \psi}{\partial y}$      $v = -\frac{\partial \psi}{\partial x}$      $v = \frac{\mu}{\rho}$

$$\Rightarrow \left[ \frac{\partial \psi}{\partial y} \frac{\partial^2 \psi}{\partial x \partial y} - \frac{\partial \psi}{\partial x} \frac{\partial^2 \psi}{\partial y^2} = v \frac{\partial^3 \psi}{\partial y^3} \right]$$

1 state variable ( $\psi$ )  
2D ( $x, y$ )

Blasius made the assumption that the boundary layer is self-similar:

- $\eta = y \left( \frac{U}{\nu x} \right)^{1/2}$
- $= \frac{y}{f(x)} \leftarrow \eta(x) = \left( \frac{\nu x}{U} \right)^{1/2}$

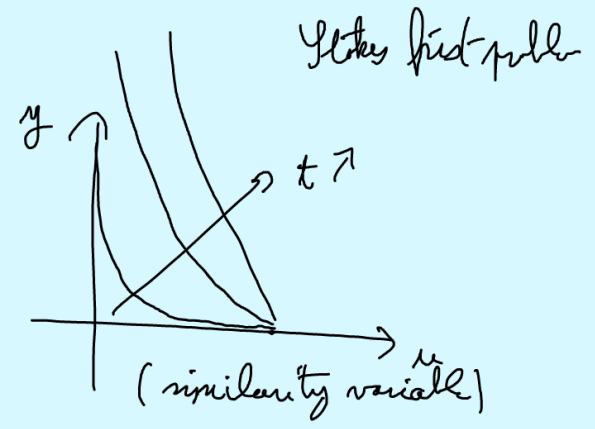
- $u = U f'$      $f' = \frac{df}{d\eta} \leftarrow$  similarity function

$\hookrightarrow u = \frac{\partial \psi}{\partial y} \Rightarrow U f' = \frac{\partial \psi}{\partial \eta} \frac{d\eta}{dy}$

$\Rightarrow \frac{\partial \psi}{\partial \eta} = U f' \delta$

$\Rightarrow \psi = U \int_{\eta} f$

$\downarrow$   
 $f(x)$



$$\begin{aligned} \cdot \frac{\partial \psi}{\partial x} &= U \delta' f + U_{\delta} \frac{\partial f}{\partial \eta} \frac{\partial \eta}{\partial x} \\ &= U \delta' f - \frac{U \eta \delta' f'}{\delta} = -v! \end{aligned}$$

$$\eta = \frac{x}{\delta}$$

$$\frac{\partial \eta}{\partial x} = -\frac{\eta \delta'}{\delta^2}$$

$$\begin{aligned} \cdot \frac{\partial \psi}{\partial y} &= U_{\delta} \frac{\partial f}{\partial \eta} \frac{\partial \eta}{\partial y} \\ &= U f' = u! \end{aligned}$$

$$\cdot \frac{\partial^2 \psi}{\partial y^2} = \frac{\partial}{\partial y} (U f')$$

$$= U \frac{\partial f'}{\partial \eta} \frac{\partial \eta}{\partial y}$$

$$= \frac{U}{\delta} f''$$

$$\cdot \frac{\partial^3 \psi}{\partial y^3} = \frac{U}{\delta^2} f'''$$

$$\cdot \frac{\partial^2 \psi}{\partial x \partial y} = \frac{\partial}{\partial x} (U f')$$

$$= U \frac{\partial f'}{\partial \eta} \frac{\partial \eta}{\partial x}$$

$$= -\frac{U \eta'}{\delta^2} f''$$

In the  $\psi$  equation:

$$U f' \left( -\frac{U f' y}{\delta^2} f'' \right) - \left[ U \delta' f - \frac{U y \delta'}{\delta} f' \right] \left( \frac{U f''}{\delta} \right) = \nu \frac{U f'''}{\delta^2}$$

$$\Rightarrow -\frac{U^2 \delta' y}{\delta^2} f' f'' - \frac{U^2 \delta'}{\delta} f f'' + \frac{U^2 y \delta'}{\delta^2} f' f'' = \nu \frac{U f'''}{\delta^2}$$

$$\Rightarrow -\frac{U^2 \delta'}{\delta} f f'' = \nu \frac{U f'''}{\delta^2}$$

$$\Rightarrow f''' + \frac{U \delta \delta'}{\nu} f f'' = 0$$

$$\delta = \left( \frac{\nu x}{U} \right)^{1/2} \Rightarrow \delta' = \frac{1}{2} \left( \frac{\nu}{x U} \right)^{1/2}$$

$$\Rightarrow \delta \delta' = \frac{1}{2} \frac{\nu}{U}$$

$$\Rightarrow \boxed{f''' + \frac{1}{2} f f'' = 0}$$

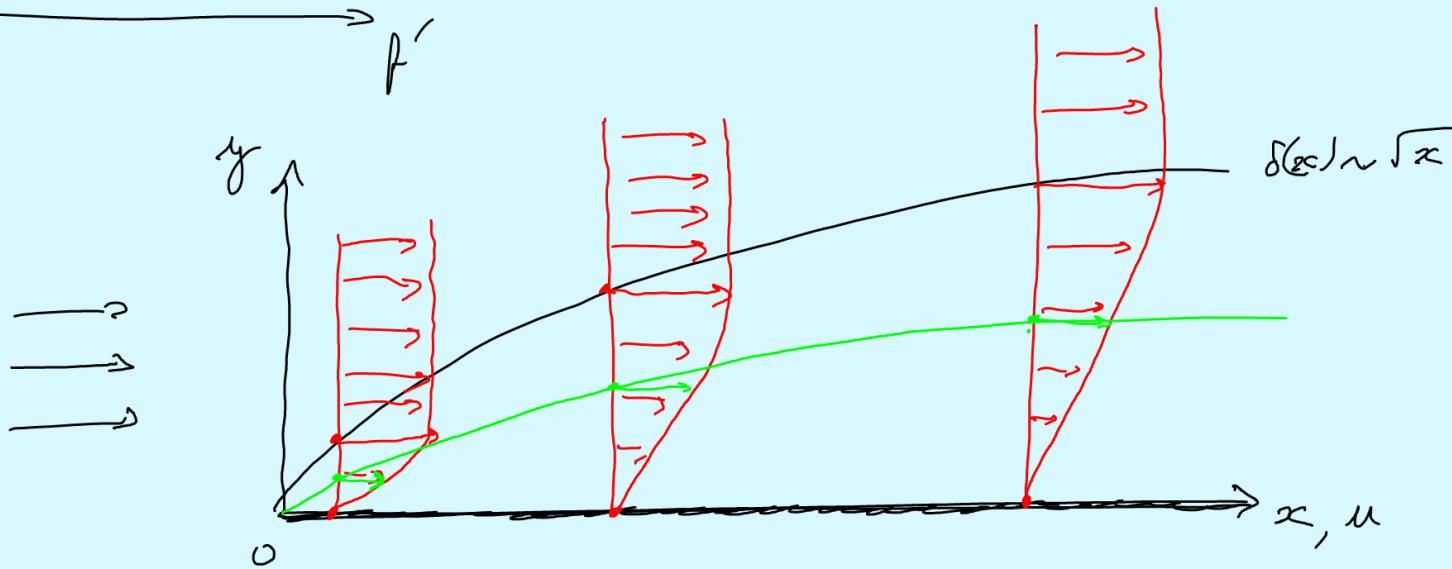
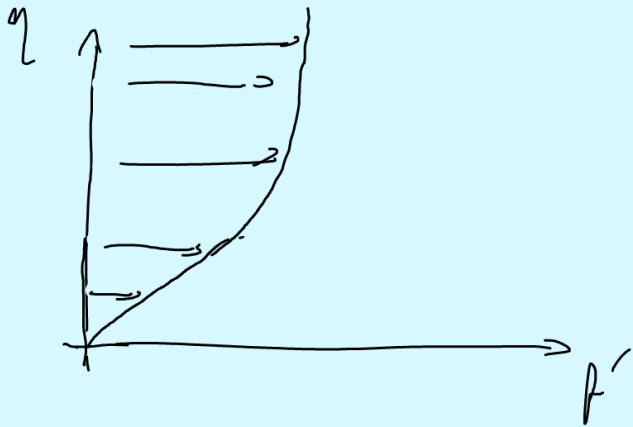
1 state variable ( $f$ )  
ID ( $\eta$ )

$$\text{BC: } \left. \begin{array}{l} y=0 \quad u=0 \\ \quad \quad v=0 \\ \\ \eta \rightarrow \infty \quad u \rightarrow U \\ \quad \quad \quad (v \rightarrow 0) \end{array} \right\} \begin{array}{l} \eta=0 \quad \beta'=0 \\ \quad \quad \beta=0 \\ \\ \eta \rightarrow \infty \quad \beta'=1 \end{array}$$

Boundary layer thickness:  $\delta: \frac{u}{U} \leq 0.99$

$$\Rightarrow f' \leq 0.99$$

$$\Rightarrow \eta \leq 5 \quad (\text{numerically})$$



$$\eta \leq 5 \Rightarrow \delta \left( \frac{U}{\nu x} \right)^{1/2} \leq 5$$

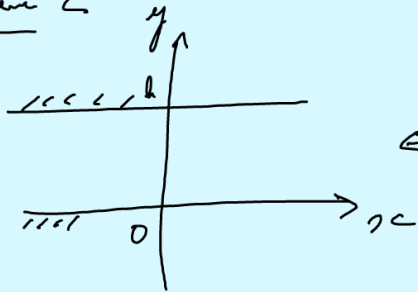
$$\Rightarrow \delta \leq 5 \left( \frac{\nu x}{U} \right)^{1/2}$$

$$\hookrightarrow \delta_{99} = 5 \left( \frac{\nu x}{U} \right)^{1/2}$$

$$\Rightarrow \frac{\delta_{99}}{x} = 5 \left( \frac{\nu}{Ux} \right)^{1/2}$$

$$\Rightarrow \frac{\delta_{99}}{x} = 5 \operatorname{Re}_x^{-1/2}$$

← boundary layer aspect ratio.

Example Sheet 4Problem 2

$$\vec{V}_p = -G \vec{e}_x$$

$\mu$  is not a function of  $x$

$$(a) \quad \text{2D: } \begin{cases} \rho \cancel{d_x \mu} + \rho \cancel{\mu d_x} + \rho \cancel{v d_y} \mu = -\cancel{d_x p} + \rho \cancel{d_x^2} \mu + \rho \cancel{d_y^2} \mu \\ \rho \cancel{d_x v} + \rho \cancel{\mu d_x v} + \rho \cancel{v d_y} v = -\cancel{d_y p} + \rho \cancel{d_x^2} v + \rho \cancel{d_y^2} v \\ \cancel{d_x \mu} + \cancel{d_y v} = 0 \end{cases}$$

$$\Rightarrow \rho d_x \mu = G + \rho d_y^2 \mu$$

$$\Rightarrow \boxed{d_x \mu = \frac{G}{\rho} + v d_y^2 \mu}$$

$$(b) \quad \mu = \mu(y) \Rightarrow \boxed{d_y^2 \mu_{SS} = -\frac{G}{\rho v}}$$

$$\Rightarrow \mu_{SS} = -\frac{G y^2}{2\rho v} + k_1 y + k_2$$

$$\text{BC: } y=0 : \mu_{SS} = 0 \Rightarrow k_2 = 0$$

$$y=h : \mu_{SS} = 0 \Rightarrow -\frac{G h^2}{2\rho v} + k_1 h = 0$$

$$\Rightarrow k_1 = \frac{Gh}{2\rho\nu}$$

$$\begin{aligned} \hookrightarrow u_{ss} &= \frac{G}{2\rho\nu} [h^2y - y^2] \\ &= \frac{Gy}{2\rho\nu} (h-y) \end{aligned}$$

$$(c) \quad u = u_{ss} + v$$

$$\partial_t u = \frac{G}{\rho} + \nu \partial_y^2 u \quad \Rightarrow \quad \partial_t (u_{ss} + v) = \frac{G}{\rho} + \nu \partial_y^2 (u_{ss} + v)$$

$$\Rightarrow \partial_t v = \underbrace{\frac{G}{\rho} + \nu \partial_y^2 u_{ss}}_{=0} + \nu \partial_y^2 v$$

$$\Rightarrow \partial_t v = \nu \partial_y^2 v$$

$$\text{BC: } \left. \begin{array}{l} u=0 \text{ at } y=0 \\ u=0 \text{ at } y=h \end{array} \right\} \Rightarrow \left\{ \begin{array}{l} u_{ss} + v = 0 \text{ at } y=0 \\ u_{ss} + v = 0 \text{ at } y=h \end{array} \right\} \Rightarrow \left\{ \begin{array}{l} v=0 \text{ at } y=0 \\ v=0 \text{ at } y=h \end{array} \right.$$

$$(d) \quad v(y,t) = Y(y)T(t)$$

$$\partial_t v = \nu \partial_y^2 v \quad \Rightarrow \quad Y T' = \nu Y'' T$$

$$\Rightarrow \frac{T'}{vT} = \frac{Y''}{Y} = k,$$

$\uparrow$                      $\uparrow$   
 (t)                    (y)

$$\Rightarrow \begin{cases} T' = vk_1 T & \Rightarrow T = k_2 \exp(vk_1 t) \\ Y'' = k_1 Y & \Rightarrow Y = k_3 \exp(\sqrt{k_1} y) + k_4 \exp(-\sqrt{k_1} y) \end{cases}$$

$$\Rightarrow v = \exp(vk_1 t) \left[ \overset{k_2 k_3}{\downarrow} k_5 \exp(\sqrt{k_1} y) + \overset{k_2 k_4}{\downarrow} k_6 \exp(-\sqrt{k_1} y) \right]$$

BC:  $v = 0$  at  $y = 0$   $\rightarrow \exp(vk_1 t) [k_5 + k_6] = 0 \Rightarrow k_5 = -k_6$   
 ( $v = 0$  at  $y = h$ )

$$\Rightarrow v = k_5 \exp(vk_1 t) \left[ \exp(\sqrt{k_1} y) - \exp(-\sqrt{k_1} y) \right]$$

$$v = 0 \text{ at } y = h \rightarrow \exp(vk_1 t) \left[ \exp(\sqrt{k_1} h) - \exp(-\sqrt{k_1} h) \right] = 0$$

$$\Rightarrow \exp(\sqrt{k_1} h) = \exp(-\sqrt{k_1} h)$$

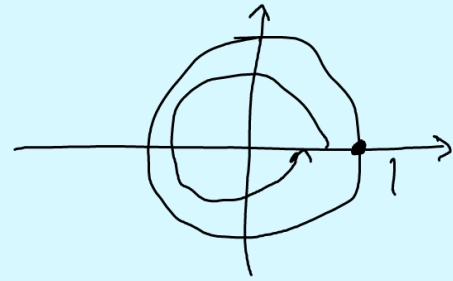
$$\Rightarrow \exp(2\sqrt{k_1} h) = 1$$

$$\Rightarrow \exp(2\sqrt{k_1} h) = e^{i2m\pi}$$



$$\Rightarrow 2\sqrt{k_{im}} h = 2im\pi \leftarrow$$

$$\Rightarrow k_{im} = -\frac{m^2\pi^2}{h^2}$$



$$\Rightarrow v_m = \underbrace{k_{5m}}_{k_{5m} 2i} \exp\left(-\sqrt{\frac{m^2\pi^2}{h^2}} t\right) \left[ \exp\left(\frac{im\pi}{h} y\right) - \exp\left(-\frac{im\pi}{h} y\right) \right]$$

$$\Rightarrow v_m = k_{6m} \exp\left(-\sqrt{\frac{m^2\pi^2}{h^2}} t\right) \sin\left(\frac{m\pi}{h} y\right)$$

$$\sin(x) = \frac{e^{ix} - e^{-ix}}{2i}$$

$$\hookrightarrow u = \frac{Gy(h-y)}{2\rho v} + \sum_{n=1}^{\infty} \underbrace{k_{6n}}_{a_n} \exp\left(-\sqrt{\frac{n^2\pi^2}{h^2}} t\right) \sin\left(\frac{n\pi}{h} y\right)$$

$$(e) u(t=0) = 0 \Rightarrow \frac{Gy(h-y)}{2\rho v} + \sum_{n=1}^{\infty} a_n \sin\left(\frac{n\pi}{h} y\right) = 0$$

$$\Rightarrow \sum_{n=1}^{\infty} a_n \sin\left(\frac{n\pi}{h} y\right) = -\frac{Gy(h-y)}{2\rho v}$$

$$\int_0^h \sin\left(\frac{m\pi}{h} y\right) \sin\left(\frac{n\pi}{h} y\right) dy = \begin{cases} 0 & \text{for } m \neq n \\ \frac{2}{h} & \text{for } m = n \end{cases} \leftarrow \text{check}$$

# Chapter 5: Potential flows

Hypotheses:

planar

incompressible

irrotational

$$\vec{u} = u(x, y) \vec{e}_x + v(x, y) \vec{e}_y$$

$$\vec{\nabla} \cdot \vec{u} = 0$$

$$\vec{\nabla} \times \vec{u} = \vec{0}$$

Do we need Navier-Stokes?

Route 1: Incompressible  $\rightarrow$  streamfunction  $\psi$

$$u = \frac{\partial \psi}{\partial y} \quad v = -\frac{\partial \psi}{\partial x}$$
$$\left( \vec{u} = \vec{\nabla} \times \psi \vec{e}_z \right)$$

$$\vec{\nabla} \cdot \vec{u} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y}$$
$$= \frac{\partial^2 \psi}{\partial x \partial y} - \frac{\partial^2 \psi}{\partial y \partial x}$$
$$= 0 \quad \checkmark$$

Irrotational:  $\vec{\nabla} \times \vec{u} = \vec{0}$

$$\Rightarrow \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = 0$$

$$\Rightarrow -\frac{\partial^2 \psi}{\partial x^2} - \frac{\partial^2 \psi}{\partial y^2} = 0$$

$$\Rightarrow \boxed{\vec{\nabla}^2 \psi = 0}$$

Route 2: Irrotational  $\rightarrow$  velocity potential  $\phi$

$$u = \frac{\partial \phi}{\partial x} \quad v = \frac{\partial \phi}{\partial y}$$

$$\vec{u} = \vec{\nabla} \phi$$

$$\vec{\nabla} \times \vec{u} = \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}$$
$$= \frac{\partial^2 \phi}{\partial x \partial y} - \frac{\partial^2 \phi}{\partial y \partial x}$$

$$= 0 \quad \checkmark \quad (\vec{\nabla} \times \vec{\nabla} \phi = \vec{0})$$

Incompressible:  $\vec{\nabla} \cdot \vec{u} = 0$

$$\Rightarrow \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\Rightarrow \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$$

$$\Rightarrow \boxed{\vec{\nabla}^2 \phi = 0}$$

Bernoulli equations : Irrotational flow  $\rightarrow$  Euler equation

$$\rho \left[ \frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} \right] = -\vec{\nabla} P - \rho g \vec{e}_z$$

vector calculus (ES 1)

$$\Rightarrow \rho \left[ \frac{\partial \vec{u}}{\partial t} - \vec{u} \times \vec{\omega} \right] = -\vec{\nabla} P - \vec{\nabla} \left( \frac{1}{2} \rho \vec{u}^2 \right) - \vec{\nabla} (\rho g z)$$

$\vec{\omega} = \vec{\nabla} \times \vec{u}$

$$\Rightarrow \rho \left[ \frac{\partial \vec{u}}{\partial t} - \vec{u} \times \vec{\omega} \right] = -\vec{\nabla} \left[ P + \frac{1}{2} \rho \vec{u}^2 + \rho g z \right]$$

(B1) Hypothesis: steady, irrotational

$$\hookrightarrow \vec{0} = -\vec{\nabla} \left[ P + \frac{1}{2} \rho \vec{u}^2 + \rho g z \right]$$

$$\Rightarrow P + \frac{1}{2} \rho \vec{u}^2 + \rho g z = \text{cst}(t)$$

$$\Rightarrow \boxed{P + \frac{1}{2} \rho \vec{u}^2 + \rho g z = \text{cst}} \quad (\text{because of steady flow})$$

$$0 = \frac{df}{dx} \Rightarrow f = \text{cst}$$

$$0 = \frac{df}{dy} \Rightarrow f = \text{cst}$$

(B2) Hypothesis: steady

$$\hookrightarrow \rho \vec{u} \times \vec{\omega} = \vec{\nabla} \left[ P + \frac{1}{2} \rho \vec{u}^2 + \rho g z \right]$$

$$\Rightarrow \underbrace{\rho \vec{u} \cdot \left[ \underbrace{\vec{u} \times \vec{\omega}}_{\perp \vec{u}} \right]}_{=0} = \vec{u} \cdot \vec{\nabla} \left[ P + \frac{1}{2} \rho \vec{u}^2 + \rho g z \right]$$

$$\Rightarrow \vec{u} \cdot \vec{\nabla} \left[ P + \frac{1}{2} \rho \vec{u}^2 + \rho g z \right] = 0$$

$$\Rightarrow \vec{u} \cdot \vec{\nabla} f = 0$$

$$\Rightarrow \vec{u} \perp \vec{\nabla} f$$

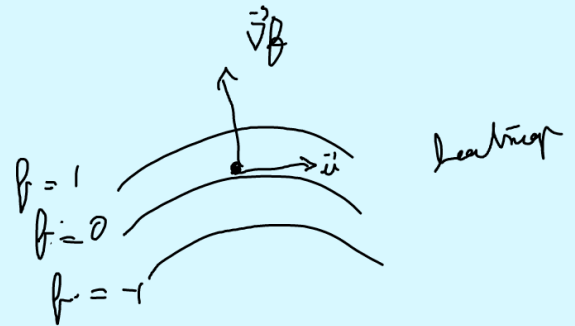
$\Rightarrow$   $f$  varies the fastest in the direction orthogonal to  $\vec{u}$

$\Rightarrow$   $\vec{u}$  is in the direction in which  $f$  does not vary

$$\Rightarrow f = \text{const}(\psi) \quad \uparrow \text{streamfunction value}$$

$$\Rightarrow \boxed{P + \frac{1}{2} \rho \vec{u}^2 + \rho g z = \text{const}(\psi)}$$

$$\boxed{P + \frac{1}{2} \rho \vec{u}^2 + \rho g z = \text{const} \quad \text{steady, along a streamline}}$$



## Complex potential:

$$f: \mathbb{C} \mapsto \mathbb{C}$$

$f$  is complex differentiable  $\Rightarrow \frac{df}{dz} = \lim_{|\delta z| \rightarrow 0} \frac{f(z+\delta z) - f(z)}{\delta z}$  has to give the same result no matter the direction of  $\delta z$ .

Let us write  $f(z) = g(x, y) + i h(x, y)$

$z = x + iy$   
 $(x, y) \in \mathbb{R}^2$

$$g: \mathbb{R}^2 \mapsto \mathbb{R}$$

$$h: \mathbb{R}^2 \mapsto \mathbb{R}$$

$\delta z = \delta x$  :  $\frac{df}{dz} = \frac{dg}{\delta x} + i \frac{dh}{\delta x}$

$\delta z = i \delta y$  :  $\frac{df}{dz} = \frac{dg}{i \delta y} + i \frac{dh}{i \delta y} = \frac{dh}{\delta y} - i \frac{dg}{\delta y}$

$f$  complex differentiable  $\Rightarrow \begin{cases} \frac{dg}{\delta x} = \frac{dh}{\delta y} & (1) \\ \frac{dh}{\delta x} = -\frac{dg}{\delta y} & (2) \end{cases}$

Cauchy-Riemann equations

$$\frac{\partial(1)}{\partial x} + \frac{\partial(2)}{\partial y} \Rightarrow \frac{\partial^2 g}{\partial x^2} + \frac{\partial^2 h}{\partial x \partial y} = \frac{\partial^2 h}{\partial x \partial y} - \frac{\partial^2 g}{\partial y^2}$$

$$\Rightarrow \frac{\partial^2 g}{\partial x^2} + \frac{\partial^2 g}{\partial y^2} = 0$$

$$\Rightarrow \vec{\nabla}^2 g = 0$$

$$\frac{\partial(1)}{\partial y} - \frac{\partial(2)}{\partial x} \Rightarrow \frac{\cancel{\partial^2 g}}{\partial x \partial y} - \frac{\partial^2 h}{\partial x^2} = \frac{\partial^2 h}{\partial y^2} + \frac{\cancel{\partial^2 g}}{\partial x \partial y}$$

$$\Rightarrow \vec{\nabla}^2 h = 0$$

We can thus introduce the complex potential  $w$  for an incompressible, irrotational, planar flow:

$$\boxed{w = \phi + i\psi}$$

complex potential
velocity potential
streamfunction

$$w \text{ is complex differentiable } \Rightarrow \vec{\nabla}^2 \phi = \vec{\nabla}^2 \psi = 0$$

$$\frac{dw}{dz} = \frac{\partial \phi}{\partial x} + i \frac{\partial \psi}{\partial x} = u - iv$$

$$= \frac{\partial \phi}{i \partial y} + i \frac{\partial \psi}{i \partial y} = \frac{\partial \psi}{\partial y} - i \frac{\partial \phi}{\partial y} = u - iv$$

$$\Rightarrow u + iv = \frac{dw}{dz}$$

$$u = \frac{\partial \phi}{\partial x} \quad v = \frac{\partial \phi}{\partial y}$$

$$u = \frac{\partial \psi}{\partial y} \quad v = -\frac{\partial \psi}{\partial x}$$

complex conjugate

$$\left\{ \begin{array}{l} u = \frac{\partial \phi}{\partial x} = \frac{\partial \psi}{\partial y} \\ v = \frac{\partial \phi}{\partial y} = -\frac{\partial \psi}{\partial x} \end{array} \right.$$

Because the Laplace equations for  $\phi$  and  $\psi$  are linear, we can use the principle of superposition:  $\phi_1$  and  $\phi_2$  solutions  $\Rightarrow \alpha\phi_1 + \beta\phi_2$  is a solution.

Building blocks of potential flows:

\* uniform flow:  $w = U_0 z e^{-i\alpha}$

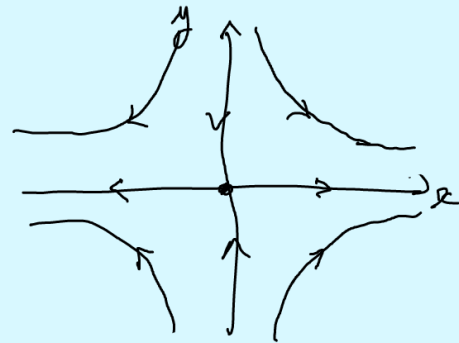
$$\frac{dw}{dz} = U_0 e^{+i\alpha}$$

$\rightarrow$  flow with speed magnitude  $U$   
angle  $\alpha$  with  $\vec{e}_x$

\* saddle point flow:  $w = Az^2$

$$\begin{aligned} \frac{dw}{dz} &= 2Az \\ &= 2Ax + 2iAy \end{aligned}$$

$$\begin{aligned} \hookrightarrow u &= 2Ax \\ v &= -2Ay \end{aligned}$$



$A > 0$

\* source/sink:  $w = A \ln z$   
 $= A \ln(re^{i\theta})$   
 $= A \ln r + iA\theta$

$\phi$        $\psi$

$$u_r = \frac{\partial \phi}{\partial r} = \frac{A}{r}$$

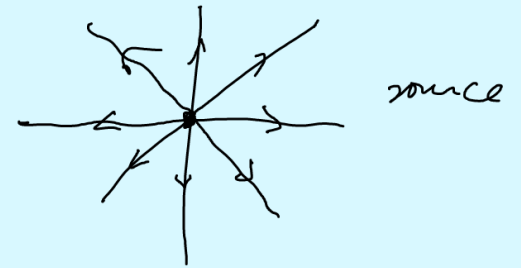
$A > 0$  source,  $A < 0$  sink

$$u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = 0$$

$$q = \int_0^{2\pi} u_r \Big|_a a d\theta$$
$$= \int_0^{2\pi} \frac{A}{a} a d\theta$$

$$= 2\pi A \quad \Rightarrow \quad A = \frac{q}{2\pi}$$

$$\boxed{w = \frac{q}{2\pi} \ln z}$$



\* vortex:

$$\boxed{w = -\frac{i\Gamma}{2\pi} \ln z}$$

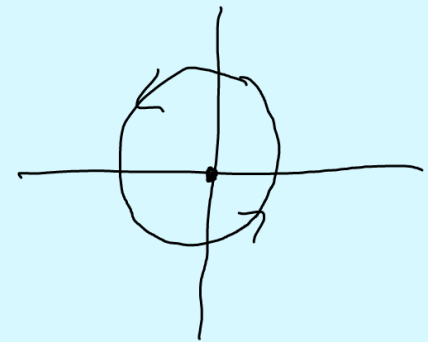
$$= -\frac{i\Gamma}{2\pi} \ln r - \frac{i\Gamma}{2\pi} i\theta$$

$$= -\frac{i\Gamma}{2\pi} \ln r + \frac{\Gamma\theta}{2\pi}$$

$\underbrace{\hspace{1.5cm}}_{\psi} \qquad \underbrace{\hspace{1.5cm}}_{\phi}$

$$u_r = \frac{\partial \phi}{\partial r} = 0$$

$$u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = \frac{\Gamma}{2\pi r} \quad \leftarrow$$





$$\left( \Gamma = \int_0^{2\pi} u_\theta |a| d\theta \right)$$

↑  
circulation

$$\begin{cases} \vec{\nabla}^2 \phi = 0 \\ \vec{\nabla}^2 \psi = 0 \end{cases}$$

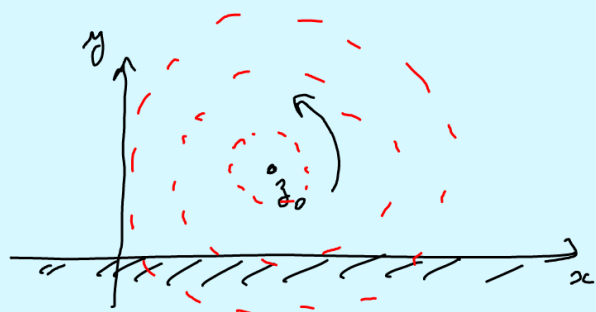
We have the equations (and the building blocks) but how to apply boundary conditions?  
What are boundary conditions?

Lecture 21

## Boundary conditions

### (1) Method of images

Imagine a vortex at  $z_0$



$$f(z) = -\frac{i\Gamma}{2\pi} \ln(z - z_0)$$

To create a wall at  $y=0$ , we apply:  $w(z) = f(z) + \overline{f(\bar{z})}$

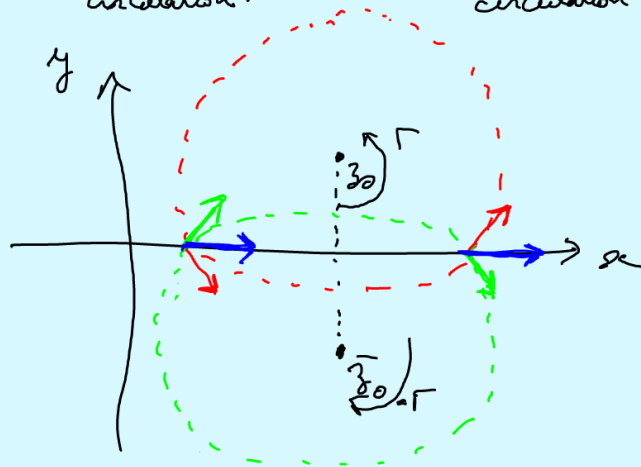
$$\begin{aligned} \text{check: } z = x &\rightarrow w(x) = f(x) + \overline{f(\bar{x})} \\ &= f(x) + \overline{f(x)} \\ &\in \mathbb{R} \end{aligned}$$

$$w = \phi + i\psi \quad \psi(x) = 0$$

Example:  $w(z) = -\frac{i\Gamma}{2\pi} \ln(z-z_0) - \frac{i\Gamma}{2\pi} \ln(\bar{z}-z_0) \Rightarrow y=0$  is a streamline

$$= -\frac{i\Gamma}{2\pi} \ln(z-z_0) + \frac{i\Gamma}{2\pi} \ln(z-\bar{z}_0)$$

$\uparrow$  vortices at  $z_0$  circulation  $\Gamma$        $\uparrow$  vortices at  $\bar{z}_0$  circulation  $-\Gamma$



To generate a wall at  $x=0$ , we apply:  $w(z) = f(z) + \overline{f(-\bar{z})}$

## (2) The Milne-Thomson circle theorem

To generate a wall at  $|z|=a$ , we apply:  $w(z) = f(z) + \overline{f\left(\frac{a^2}{z}\right)}$  ←

at the wall:  $z = a e^{i\theta} \rightarrow w(a e^{i\theta}) = f(a e^{i\theta}) + \overline{f\left(\frac{a^2}{a e^{i\theta}}\right)}$

$$= f(a e^{i\theta}) + \overline{f\left(\frac{a^2}{a e^{-i\theta}}\right)}$$

$$= f(a e^{i\theta}) + \overline{f(a e^{i\theta})}$$

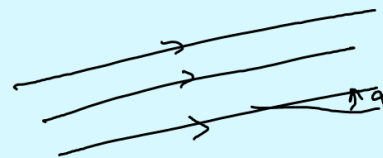
$$\in \mathbb{R}$$

↳ Therefore,  $|z|=a$  is a streamline (or a wall)

Example: flow past a cylinder

step 1: generate a flow

$$f(z) = U_0 z e^{-i\alpha}$$

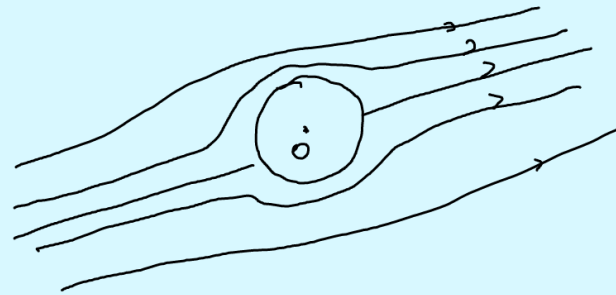


step 2: Milne-Thomson theorem

$$w(z) = U_0 z e^{-i\alpha} + \overline{U_0 \frac{a^2}{z} e^{-i\alpha}}$$

$$= U_0 z e^{-i\alpha} + U_0 \frac{a^2}{z} e^{i\alpha}$$

$$= U_0 \left[ z e^{-i\alpha} + \frac{a^2}{z} e^{i\alpha} \right] \leftarrow$$



step 3: add circulation:  $w(z) = U_0 \left[ z e^{-i\alpha} + \frac{a^2}{z} e^{i\alpha} \right] - \frac{i\Gamma}{2\pi} \ln z$

---

### (3) Conformal mapping



First, we generate a uniform flow:  $w(z) = U_0 z$

To create the above corner, we apply:  $Z = z^{\alpha/\pi} \mapsto z = Z^{\pi/\alpha}$

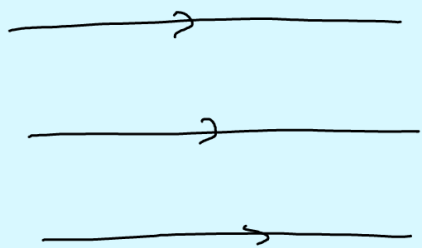
Here:  $W(Z) = U_0 Z^{\pi/\alpha}$

The  $y=0$  axis can be parameterized by:  $z = r e^{i\theta} \rightarrow \theta = 0$   
 $\searrow \theta = \pm \pi$

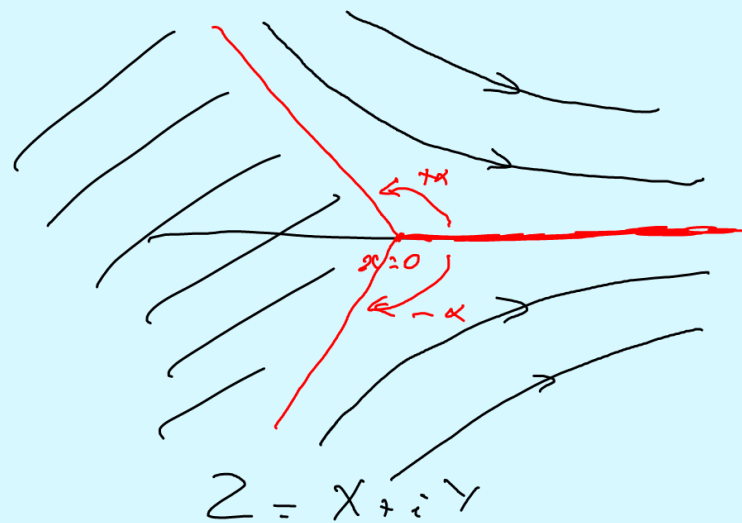
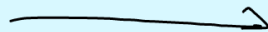
\*  $\theta = 0$ :  $z = r e^{i\theta} \rightarrow Z = r e^{i\theta/\pi} \leftarrow$   
 $= r e^{i\theta/\pi} \rightarrow$  remains  $y=0, x>0$

\*  $\theta = \pi$ :  $Z = r e^{i\theta/\pi} = r e^{i\pi} \rightarrow$  rotated to make an angle  $\alpha$  with  $\theta=0$ .

\*  $\theta = -\pi$ :  $Z = r e^{i\theta/\pi} = r e^{-i\pi} \rightarrow$  rotated to make an angle  $-\alpha$  with  $\theta=0$



$$z = x + iy$$



$$Z = X + iY$$